

Fluid flow at the interface between elastic solids with randomly rough surfaces

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I study fluid flow at the interface between elastic solids with randomly rough surfaces. I use the contact mechanics model of Persson to take into account the elastic interaction between the solid walls and the Bruggeman effective medium theory to account for the influence of the disorder on the fluid flow. I calculate the flow tensor which determines the pressure flow factor and, e.g., the leak-rate of static seals. I show how the perturbation treatment of Tripp can be extended to arbitrary order in the ratio between the root-mean-square roughness amplitude and the average interfacial surface separation. I introduce a matrix $D(\zeta)$, determined by the surface roughness power spectrum, which can be used to describe the anisotropy of the surface at any magnification ζ . I present results for the asymmetry factor $\gamma(\zeta)$ (generalized Peklenik number) for grinded steel and sandblasted PMMA surfaces.

1. Introduction

The influence of surface roughness on fluid flow at the interface between solids in stationary or sliding contact is a topic of great importance both in Nature and Technology. Technological applications includes leakage of seals, mixed lubrication, and removal of water from the tire-road footprint. In Nature fluid removal (squeeze-out) is important for adhesion and grip between the tree frog or Gecko adhesive toe pads and the countersurface during raining, and for cell adhesion.

Almost all surfaces in Nature and most surfaces of interest in Tribology have roughness on many different length scales, sometimes extending from atomic distances (~ 1 nm) to the macroscopic size of the system which could be of order ~ 1 cm. Often the roughness is fractal-like so that when a small region is magnified (in general with different magnification in the parallel and orthogonal directions) it “looks the same” as the unmagnified surface.

Most objects produced in engineering have some particular macroscopic shape characterized by a radius of curvature (which may vary over the surface of the solid) e.g., the radius R of a cylinder in an engine. In this case the surface may appear perfectly smooth to the naked eye but at short enough length scale, in general much smaller than R , the surface will exhibit strong irregularities (surface roughness). The surface roughness power spectrum $C(\mathbf{q})$ of such a surface will exhibit a roll-off wavelength $\lambda_0 \ll R$ (related to the roll-off wavevector $q_0 = 2\pi/\lambda_0$) and will appear smooth (except for the macroscopic curvature R) on length scales much longer than λ_0 . In this case, when studying the fluid flow between two macroscopic solids, one may replace the microscopic equations of fluid dynamics with effective equations describing the average fluid flow on length scales much larger than λ_0 , and which can be used to study, e.g., the lubrication of the cylinder in an engine. This approach of eliminating or integrating out short length scale degrees of freedom to obtain effective equations of motion which describes the long distance (or slow) behavior is a very general and powerful concept often used in Physics.

In the context of fluid flow at the interface between closely spaced solids with surface roughness, Patir and Cheng[1, 2] have showed how the Navier-Stokes equations of fluid dynamics can be reduced to effective equations of motion involving locally averaged fluid pressure and flow velocities. In the effective equation occur so called flow factors, which are functions of the locally averaged interfacial surface separation \bar{u} . They showed how the flow factors can be determined by solving numerically the fluid flow in small rectangular units with linear size of order (or larger than) the roll-off wavelength λ_0 introduced above. However, with the present speed (and memory) limitations of computers fully converged solutions using this approach can only take into account roughness over two or at most three decades in length scale. In addition, Patir and Cheng did not include the long-range elastic deformations of the solid walls in the analysis. Later studies have attempted to include elastic deformation using the contact mechanics model of Greenwood-Williamson (GW)[3], but it is now known that this theory (and other asperity contact models [4]) does not correctly describe contact mechanics because of the neglect of the long range elastic coupling between the asperity contact regions[5, 6]. In particular, the relation between the average interfacial separation \bar{u} and the squeezing pressure p , which is very important for the fluid flow problem, is incorrectly described by the GW model [the GW model predict asymptotically (for large \bar{u}) $p \sim \exp(-a\bar{u}^2)$, while the exact result[7–9] for randomly rough surfaces is $p \sim \exp(-b\bar{u})$, where a and b are constants determined by the nature of the surface roughness].

The paper by Patir and Cheng was followed by many other studies of how to eliminating or integrate out the surface roughness in fluid flow problems (see, e.g., the work by Sahlin et al.[10]). Most of these theories involves solving numerically for the fluid flow in rectangular interfacial units and, just as in the Patir and Cheng approach, cannot include roughness on more than ~ 2 decades in length scale. In addition, in some of the studies the measured roughness topography must be “processed” in a

non-trivial way in order to obey periodic boundary conditions (which is necessary for the Fast Fourier Transform method used in some of these studies).

Tripp[11] has presented an analytical derivation of the flow factors for the case where the separation between the surfaces is so large that no direct solid-solid contact occurs. He obtained the flow factors to first order in $\langle h^2 \rangle / \bar{u}^2$, where $\langle h^2 \rangle$ is the ensemble average of the square of the roughness amplitude and \bar{u} the average surface separation. This result is of great conceptual importance, but of minor practical importance as the influence of the surface roughness on the fluid flow becomes important only when direct solid-solid contact occur.

Many surfaces of practical importance have roughness with isotropic statistical properties, e.g., sandblasted surfaces or surfaces coated with particles typically bound by a resin to an otherwise flat surface, e.g., sandpaper surfaces. However some surfaces of engineering interest have surface roughness with anisotropic statistical properties, e.g., surfaces which have been polished or grinded in one direction. The theories of Patir and Chen[1, 2] and of Tripp[11] can be applied also to surfaces with anisotropic statistical properties. The surface anisotropy is usually characterized by a single number, the so called Peklenik number γ , which is the ratio between the decay length of the height-height correlation function $\langle h(x, y)h(0, 0) \rangle$ along the x and y -directions, i.e., $\gamma = \xi_x / \xi_y$ where $\langle h(\xi_x, 0)h(0, 0) \rangle = \langle h(0, 0)h(0, 0) \rangle / 2$ and $\langle h(0, \xi_y)h(0, 0) \rangle = \langle h(0, 0)h(0, 0) \rangle / 2$. Here it has been assumed that the x -axis is oriented along one of the principal direction of the anisotropic surface roughness. However, the anisotropy properties of a surface may depend on the resolution (or magnification) which is not taken into account in this picture.

In this paper I will present a new approach to calculate the fluid flow at the interface between two elastic solids with randomly rough surfaces. The present treatment is based on a recently developed theory for calculating the leak rate of stationary seals[12]. The theory use the contact mechanics theory of Persson[13, 14] in combination with the Bruggeman effective medium theory to calculate the fluid conductivity tensor. In this paper we will generalize the treatment presented in Ref. [12] to surfaces with random roughness with anisotropic statistical properties. We also introduce a generalized Peklenik number $\gamma(\zeta)$ which depends on the magnification γ . Thus the theory takes into account that the anisotropy properties of the surface roughness may depend on the magnification under which the surface is observed. We present results for how $\gamma(\zeta)$ depends on ζ for a grinded steel surface studied using Atomic Force Microscopy and Scanning Tunneling Microscopy, and for a sandblasted PMMA surface studied using an optical technique. As an illustration we calculate the pressure flow factor for surfaces with anisotropic properties. We emphasize that the present treatment accurately accounts for surface roughness on

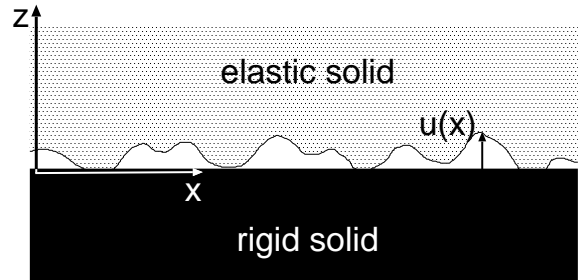


FIG. 1: An elastic solid with a rough surface in contact with a rigid solid with a flat surface.

arbitrary many decades in length scale, and a full calculation typically takes less than a minute on a normal PC. In particular, the presented theory should be very useful for gaining a quick insight into what are the most important length scales in the problem under study.

This paper is organized as follows: In Sec. 2 we briefly review the basic equations of fluid dynamics and describe some simplifications which are valid in the present case. In Sec. 3 and Appendix A I show how the perturbation treatment of Tripp can be extended to arbitrary order in $\langle h^2 \rangle / \bar{u}^2$. This treatment may not be so important for the fluid flow we consider as it is necessary to take into account that asperity contact occur already for relative small values of $\langle h^2 \rangle / \bar{u}^2$, but the approach may find applications in other contexts. In addition, the solution we present in wavevector space differ from the treatment of Tripp and leads directly to a matrix $D(\zeta)$ which we used to describe the anisotropy of the surface at any magnification ζ . In Sec. 4 we define $D(\zeta)$ and present results for how the asymmetry factor $\gamma(\zeta)$ (generalized Peklenik number) depends on the magnification ζ . In Sec. 5 we briefly review the contact mechanics model we use. In Sec. 6 we describe the critical junction theory for the flow factor, and in Sec. 7 and 8 we show how the Bruggeman effective medium theory can be used in combination with the contact mechanics theory to calculate the fluid flow tensor which determines the pressure flow factor and, e.g., the leak-rate of stationary seals. Sec. 9 contains the summary.

2. Fluid flow between solids with random surface roughness

Consider two elastic solids with randomly rough surfaces. Even if the solids are squeezed in contact, because of the surface roughness there will in general be non-contact regions at the interface and, if the squeezing force is not too large, there will exist non-contact channels from one side to the other side of the nominal contact region. We consider now fluid flow at the interface between the solids. We assume that the fluid is Newtonian and that the fluid velocity field $\mathbf{v}(\mathbf{x}, t)$ satisfies the

Navier-Stokes equation:

$$\frac{\partial \mathbf{v}}{\partial t} + \mathbf{v} \cdot \nabla \mathbf{v} = -\frac{1}{\rho} \nabla p + \nu \nabla^2 \mathbf{v}$$

where $\nu = \eta/\rho$ is the kinetic viscosity and ρ the mass density. For simplicity we will also assume an incompressible fluid so that

$$\nabla \cdot \mathbf{v} = 0$$

We assume that the non-linear term $\mathbf{v} \cdot \nabla \mathbf{v}$ can be neglected (which correspond to small inertia and small Reynolds number), which is usually the case in fluid flow between narrowly spaced solid walls. For simplicity we assume the lower solid to be rigid with a flat surface, while the upper solid is elastic with a rough surface. Introduce a coordinate system xyz with the xy -plane in the surface of the lower solid and the z -axis pointing towards the upper solid, see Fig. 1. The upper solid moves with the velocity \mathbf{v}_0 parallel to the lower solid. Let $u(x, y, t)$ be the separation between the solid walls and assume that the slope $|\nabla u| \ll 1$. We also assume that $u/L \ll 1$, where L is the linear size of the nominal contact region. In this case one expect that the fluid velocity varies slowly with the coordinates x and y as compared to the variation in the orthogonal direction z . Assuming a slow time dependence the Navier Stokes equations reduces to

$$\eta \frac{\partial^2 \mathbf{v}}{\partial z^2} = \nabla p$$

Here and in what follows $\mathbf{v} = (v_x, v_y)$, $\mathbf{x} = (x, y)$ and $\nabla = (\partial_x, \partial_y)$ are two-dimensional vectors. Note that $v_z \approx 0$ and that $p(\mathbf{x})$ is independent of z to a good approximation. The solution to the equations above can be written as

$$\mathbf{v} = \frac{1}{2\eta} z(z - u(\mathbf{x})) \nabla p + \frac{z}{u(\mathbf{x})} \mathbf{v}_0$$

so that $\mathbf{v} = 0$ on the solid wall $z = 0$ and $\mathbf{v} = \mathbf{v}_0$ for $z = u(\mathbf{x})$. Integrating over z (from $z = 0$ to $z = u(\mathbf{x})$) gives the fluid flow vector

$$\mathbf{J} = -\frac{u^3(\mathbf{x})}{12\eta} \nabla p + \frac{1}{2} u(\mathbf{x}) \mathbf{v}_0 \quad (1)$$

Mass conservation demand that

$$\frac{\partial u(\mathbf{x}, t)}{\partial t} + \nabla \cdot \mathbf{J} = 0$$

where the interfacial separation $u(\mathbf{x}, t)$ is the volume of fluid per unit area. In this last equation we have allowed for a slow time dependence of $u(\mathbf{x}, t)$ as would be the case, e.g., during fluid squeeze-out from the interfacial region between two solids. However, in this paper we will only focus on the case where u is time independent

so that $\nabla \cdot \mathbf{J} = 0$. This case is relevant for, e.g., fluid leakage in stationary seals.

3. Perturbation treatment

Here we show how one can obtain an effective flow equation by integrating out the short-wavelength roughness. We first re-derive the (first order) expansion result of Tripp in wavevector space. After that we present the results of a Renormalization Group type of treatment (the derivation is presented in Appendix A). The treatment presented here does not take into account the elastic interaction between the solid walls and is therefore strictly valid only for large enough average wall-wall separation.

Let $u(\mathbf{x}) = \bar{u} + h(\mathbf{x})$ denote the local surface separation, where $\bar{u} = \langle u \rangle$ is the average separation ($\langle \dots \rangle$ stands for ensemble averaging), and $h(\mathbf{x})$ is the contribution from the surface roughness with $\langle h \rangle = 0$. In this section we assume $h/\bar{u} \ll 1$ and perform a perturbation expansion in the small parameter h/\bar{u} . Let us write the fluid pressure as

$$p = p_0 + p_1 + p_2 + \dots$$

where p_0 is the pressure to zero order in h (so that $p_0 = \langle p_0 \rangle$), p_1 to first order in h and so on. The fluid flow current is given by

$$\mathbf{J} = -\frac{u^3}{12\eta} \nabla p + \frac{1}{2} u \mathbf{v}$$

Thus to second order in h we get

$$\begin{aligned} \mathbf{J} = & -\frac{\bar{u}^3}{12\eta} \nabla (p_0 + p_1 + p_2) \\ & -\frac{3\bar{u}^2 h}{12\eta} \nabla (p_0 + p_1) - \frac{3\bar{u} h^2}{12\eta} \nabla p_0 + \frac{1}{2} (\bar{u} + h) \mathbf{v} \end{aligned} \quad (2)$$

The ensemble average of this equation gives

$$\begin{aligned} \langle \mathbf{J} \rangle = & -\frac{\bar{u}^3}{12\eta} \nabla \langle p_0 + p_1 + p_2 \rangle \\ & -\frac{3\bar{u}^2}{12\eta} \langle h \nabla p_1 \rangle - \frac{3\bar{u} \langle h^2 \rangle}{12\eta} \nabla p_0 + \frac{1}{2} \bar{u} \mathbf{v} \end{aligned} \quad (3)$$

where we have used that $\langle h \rangle = 0$. Using that

$$\nabla \cdot \mathbf{J} = 0$$

we get from (2) to zero order in h :

$$\nabla^2 p_0 = 0.$$

The first order contribution gives

$$-\frac{\bar{u}^3}{12\eta} \nabla^2 p_1 - \frac{3\bar{u}^2}{12\eta} \nabla \cdot (h \nabla p_0) + \frac{1}{2} \mathbf{v} \cdot \nabla h = 0 \quad (4)$$

We define

$$p_1(\mathbf{q}) = \frac{1}{(2\pi)^2} \int d^2x p_1(\mathbf{x}) e^{-i\mathbf{q}\cdot\mathbf{x}}$$

$$p_1(\mathbf{x}) = \int d^2q p_1(\mathbf{q}) e^{i\mathbf{q}\cdot\mathbf{x}}$$

and similar for $h(\mathbf{x})$. Substituting these results in (4) gives

$$\frac{\bar{u}^3}{12\eta} q^2 p_1(\mathbf{q}) - \frac{3\bar{u}^2}{12\eta} h(\mathbf{q})(i\mathbf{q}) \cdot \nabla p_0 + \frac{1}{2} \mathbf{v} \cdot (i\mathbf{q}) h(\mathbf{q}) = 0 \quad (5)$$

or

$$p_1(\mathbf{q}) = \frac{3}{\bar{u}q^2} h(\mathbf{q})(i\mathbf{q}) \cdot \nabla p_0 - \frac{6\eta}{\bar{u}^3 q^2} \mathbf{v} \cdot (i\mathbf{q}) h(\mathbf{q}) \quad (6)$$

Next, note that

$$\begin{aligned} \langle h(\mathbf{q}) h(\mathbf{q}') \rangle &= \frac{1}{(2\pi)^4} \int d^2x d^2x' \langle h(\mathbf{x}) h(\mathbf{x}') \rangle e^{i\mathbf{q}\cdot\mathbf{x} + i\mathbf{q}'\cdot\mathbf{x}'} \\ &= \frac{1}{(2\pi)^4} \int d^2x d^2x' \langle h(\mathbf{x} - \mathbf{x}') h(\mathbf{0}) \rangle e^{i\mathbf{q}\cdot\mathbf{x} + i\mathbf{q}'\cdot\mathbf{x}'} \\ &= \frac{1}{(2\pi)^4} \int d^2x d^2x' \langle h(\mathbf{x} - \mathbf{x}') h(\mathbf{0}) \rangle e^{i\mathbf{q}\cdot(\mathbf{x} - \mathbf{x}') + i(\mathbf{q}' + \mathbf{q})\cdot\mathbf{x}'} \\ &= \frac{1}{(2\pi)^4} \int d^2x d^2x' \langle h(\mathbf{x}) h(\mathbf{0}) \rangle e^{i\mathbf{q}\cdot\mathbf{x} + i(\mathbf{q}' + \mathbf{q})\cdot\mathbf{x}'} \\ &= \frac{1}{(2\pi)^2} \int d^2x \langle h(\mathbf{x}) h(\mathbf{0}) \rangle e^{i\mathbf{q}\cdot\mathbf{x}} \delta(\mathbf{q} + \mathbf{q}') \\ &= C(\mathbf{q}) \delta(\mathbf{q} + \mathbf{q}') \end{aligned}$$

Using this equation and (6) gives

$$\begin{aligned} \langle h \nabla p_1 \rangle &= \int d^2q d^2q' (i\mathbf{q}') \langle h(\mathbf{q}) p_1(\mathbf{q}') \rangle e^{i(\mathbf{q} + \mathbf{q}')\cdot\mathbf{x}} \\ &= \int d^2q C(\mathbf{q}) \frac{\mathbf{q}\mathbf{q}}{q^2} \cdot \left(\frac{6\eta}{\bar{u}^3} \mathbf{v} - \frac{3}{\bar{u}} \nabla p_0 \right) \end{aligned}$$

Substituting this result in (3) gives

$$\langle \mathbf{J} \rangle = -\frac{1}{12\eta} A(\bar{u}) \nabla \bar{p} + \frac{1}{2} B(\bar{u}) \mathbf{v} \quad (7)$$

where $\bar{p} = \langle p_0 + p_1 + p_2 \rangle$, and where the 2×2 matrices A and B can be written as $A = \bar{u}^3 \phi_p$ and $B = \bar{u} \phi_s$ with the flow factor matrices

$$\phi_p = 1 + \frac{3}{\bar{u}^2} \left(\langle h^2 \rangle - 3 \int d^2q C(\mathbf{q}) \frac{\mathbf{q}\mathbf{q}}{q^2} \right)$$

$$= 1 + \frac{3\langle h^2 \rangle}{\bar{u}^2} (1 - 3D), \quad (8)$$

and

$$\phi_s = 1 - \frac{3}{\bar{u}^2} \int d^2q C(\mathbf{q}) \frac{\mathbf{q}\mathbf{q}}{q^2} = 1 - \frac{3\langle h^2 \rangle}{\bar{u}^2} D. \quad (9)$$

Here we have defined the 2×2 matrix

$$D = \frac{\int d^2q C(\mathbf{q}) \mathbf{q}\mathbf{q}/q^2}{\int d^2q C(\mathbf{q})}$$

where q_0 is the smallest surface roughness wavevector. For roughness with isotropic statistical properties, $D_{ij} = 1/2$ in which case (8) and (9) becomes

$$\phi_p = \phi_s = 1 - \frac{3}{2} \frac{\langle h^2 \rangle}{\bar{u}^2}. \quad (10)$$

In deriving (7) we have used that to order h^2 one can replace terms like $h^2 \nabla p_0$ with $h^2 \nabla \bar{p}$.

In the derivation above we calculated the pressure and shear flow factors to first order in $\langle h^2 \rangle / \bar{u}^2$. In principle it is possible to extend the perturbation expansion to calculate higher order terms in $\langle h^2 \rangle / \bar{u}^2$. This will result in higher order correlation functions, e.g., $\langle h_1 h_2 h_3 h_4 \rangle$ (where $h_1 = h(\mathbf{q}_1)$ and so on), but if the surface is randomly rough then these higher order correlation functions can be decomposed into a sum of products of pair correlation functions, e.g.,

$$\langle h_1 h_2 h_3 h_4 \rangle = \langle h_1 h_2 \rangle \langle h_3 h_4 \rangle + \langle h_1 h_3 \rangle \langle h_2 h_4 \rangle + \langle h_1 h_4 \rangle \langle h_2 h_3 \rangle$$

Thus, all terms in the perturbation expansion will only involve the pair correlation function $C(\mathbf{q})$. We empathize that this is the case only for randomly rough surfaces where the phase of the different plane-wave components in the Fourier decomposition of $h(\mathbf{x})$ are uncorrelated. However, already the calculation of the second order term in the expansion of the flow factors in $\langle h^2 \rangle / \bar{u}^2$ becomes very cumbersome. In Appendix A we present a much simple and more powerful approach, which is in the spirit of the Renormalization Group (RG) procedure. Thus we eliminate or integrate out the surface roughness components in steps and obtain a set of RG flow equations describing how the effective fluid equation evolves as more and more of the surface roughness components are eliminated.

Assume that after eliminating all the surface roughness components with wavevector $|\mathbf{q}| = q > \zeta q_0$ the fluid current takes the form

$$\mathbf{J} = -\frac{1}{12\eta} A(u, \zeta) \nabla p + \frac{1}{2} B(u, \zeta) \mathbf{v} \quad (11)$$

where A and B are 2×2 matrices. In Appendix A we show that $A(u, \zeta)$ and $B(u, \zeta)$ satisfies

$$\frac{\partial A}{\partial \zeta} = \left[\frac{1}{2} A''(u, \zeta) - A'(u, \zeta) M A'(u, \zeta) \right] \frac{d}{d\zeta} \langle h^2 \rangle_\zeta \quad (12)$$

$$\frac{\partial B}{\partial \zeta} = \left[\frac{1}{2} B''(u, \zeta) - A'(u, \zeta) M B'(u, \zeta) \right] \frac{d}{d\zeta} \langle h^2 \rangle_\zeta \quad (13)$$

where $A' = \partial A / \partial u$ and so on, and where the 2×2 matrix $M \sim A^{-1}$ is defined in Appendix A. Here $\langle h^2 \rangle_\zeta$ is the mean of the square of the roughness amplitude including only the roughness components with wavevector $q > \zeta q_0$ which can be written as

$$\langle h^2 \rangle_\zeta = \int_{q > \zeta q_0} d^2 q C(\mathbf{q}) \quad (14)$$

If we assume that $D(\zeta)$ (defined in Appendix A and in Sec. 4) is independent of ζ , it is easy to solve these equations using perturbation theory to arbitrary order in the surface roughness amplitude h . As an example, for random roughness with isotropic statistical properties one obtain to second order in $\langle h^2 \rangle / \bar{u}^2$ (see Appendix A):

$$A = u^3 \left(1 - \frac{3}{2} \frac{\langle h^2 \rangle_\zeta}{u^2} - \frac{9}{8} \frac{\langle h^2 \rangle_\zeta^2}{u^4} \right) \quad (15)$$

$$B = u \left(1 - \frac{3}{2} \frac{\langle h^2 \rangle_\zeta}{u^2} - \frac{21}{8} \frac{\langle h^2 \rangle_\zeta^2}{u^4} \right) \quad (16)$$

The terms to linear order in $\langle h^2 \rangle$ in these expressions agree with the result of Tripp. He compared his expansion results with the numerical results of Patir and Cheng and found that the expression for A (or ϕ_p) and B (or ϕ_s) agree rather well with the numerical results for $\langle h^2 \rangle^{1/2} / \bar{u} < 3$ and < 6 , respectively. For the latter case our second order contribution to B improves the agreement between numerical results and the expansion result but for $\langle h^2 \rangle^{1/2} / \bar{u} < 3$ the direct wall-wall interaction becomes so important that the expansion result (which neglect this interaction) cannot be used.

4. Surfaces with anisotropic statistical properties

As discussed in the introduction, surfaces with anisotropic statistical properties are usually characterized by the Peklenik number $\gamma = \xi_x / \xi_y$, which is the ratio between characteristic correlation length ξ_x and ξ_y , defined as the distances along the x and y -axis where the height-height correlation function $\langle h(x, y) h(0, 0) \rangle$ has decayed to half of its initial value. However, for most real surfaces $\gamma(\zeta)$ will depend on the magnification or length-scale under consideration. Here we propose to obtain $\gamma(\zeta)$ from the surface roughness power spectrum $C(q_x, q_y)$ as follows:

The surface roughness power spectrum $C(\mathbf{q})$ is defined by

$$C(\mathbf{q}) = \frac{1}{(2\pi)^2} \int d^2 x \langle h(\mathbf{x}) h(\mathbf{0}) \rangle e^{i\mathbf{q} \cdot \mathbf{x}}$$

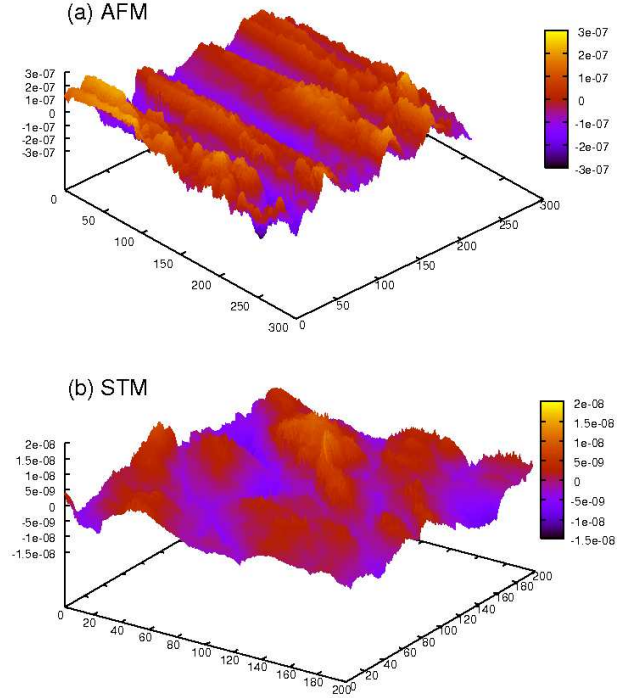


FIG. 2: Surface topography of a grinded steel surface obtained using (a) Atomic Force Microscopy (AFM) ($10\mu\text{m} \times 10\mu\text{m}$) and (b) Scanning Tunneling Microscopy (STM) ($0.1\mu\text{m} \times 0.1\mu\text{m}$).

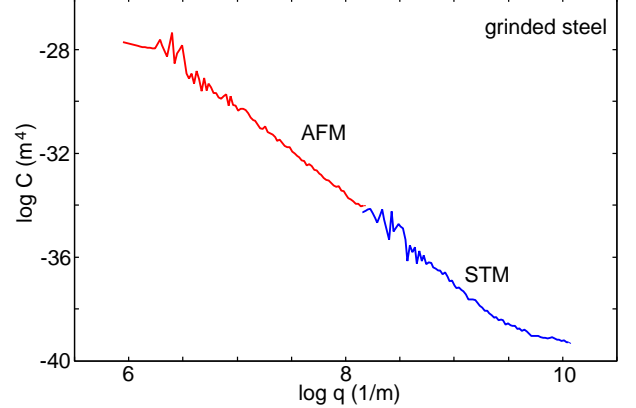


FIG. 3: The (angular averaged) surface roughness power spectrum $C(q)$ calculated from the AFM and the STM surface topography data shown in Fig. 2.

We can write

$$C(\mathbf{x}) = \langle h(\mathbf{x}) h(\mathbf{0}) \rangle = \int d^2 q C(\mathbf{q}) e^{-i\mathbf{q} \cdot \mathbf{x}}$$

We also define

$$C(\mathbf{x}, \zeta) = \int_0^{2\pi} d\phi C(\mathbf{q}) e^{-i\mathbf{q} \cdot \mathbf{x}}$$

where $\mathbf{q} = \zeta q_0 (\cos\phi, \sin\phi)$. Now consider the closed con-

tour defined by

$$C(\mathbf{x}, \zeta) = C(\mathbf{0}, \zeta)/2$$

We now fit this contour to the quadratic function $f(\mathbf{x}) = a_{ij}x_ix_j + b_ix_i + c$. The function $a_{ij}x_ix_j = \text{const.}$ describes an ellipse which in general has its major axis rotated by some angle ψ relative to the x -axis. We define γ as the ratio between the major and minor ellipse axis, and obtain both $\gamma(\zeta)$ and the rotation angle $\psi(\zeta)$, both of which depend on the magnification ζ .

Another way to determine an effective $\gamma(\zeta)$ is as follows: Consider the tensor (see also Appendix A)

$$D(\zeta) = \frac{\int_0^{2\pi} d\phi C(\mathbf{q})\mathbf{q}\mathbf{q}/q^2}{\int_0^{2\pi} d\phi C(\mathbf{q})} \quad (17a)$$

where $\mathbf{q} = \zeta q_0(\cos\phi, \sin\phi)$. If $D(\zeta)$ is independent of ζ then this definition is identical to

$$D = \frac{\int d^2q C(\mathbf{q})\mathbf{q}\mathbf{q}/q^2}{\int d^2q C(\mathbf{q})} \quad (17b)$$

which appeared already in the perturbation calculation in Sec. 3. Note that $D_{11} + D_{22} = \text{Tr}D = 1$ and that the D is symmetric and can be diagonalized. For example, suppose $C(\mathbf{q}) = f(\alpha_x q_x^2 + \alpha_y q_y^2)$ and that the \mathbf{q} -integrals in (17b) are over the whole \mathbf{q} -plane. For this case we get after some simplifications

$$D = \frac{1}{2\pi} \int_0^{2\pi} d\phi \frac{\hat{x}\hat{x}\cos^2\phi + \hat{y}\hat{y}\gamma^2\sin^2\phi}{\cos^2\phi + \gamma^2\sin^2\phi} \quad (18)$$

where $\gamma^2 = \alpha_x/\alpha_y$. Performing the integral gives $D_{11} = 1/(1 + \gamma)$ and $D_{22} = \gamma/(1 + \gamma)$. Note that in this case $|D| = D_{11}D_{22} = \gamma/(1 + \gamma)^2$ where $|D|$ is the determinant of the matrix D . This equation has two solutions, γ and $1/\gamma$ where

$$\gamma = \frac{1}{2|D|} \left[1 - (1 - 4|D|)^{1/2} \right] - 1 \quad (19)$$

Note that this definition of γ is independent of the coordinate system used since the determinant is invariant under rotations (orthogonal transformations). Note also that for a surface with isotropic statistical properties from (17) $D_{ij} = \delta_{ij}/2$ so that $|D| = 1/4$ and (19) reduces to $\gamma = 1$ as it should. The angle ψ between the major axis of the ellipse and the x -axis of the coordinate system depends, of course, on the coordinate system, and is given by

$$\tan\psi = c \pm (1 + c^2)^{1/2} \quad (20)$$

where $c = (D_{22} - D_{11})/(2D_{12})$.

In Fig. 2 we show the surface topography of a grinded steel surface as obtained using (a) Atomic Force Microscopy (AFM) ($10\mu\text{m} \times 10\mu\text{m}$) and (b) Scanning Tunneling Microscopy (STM) ($0.1\mu\text{m} \times 0.1\mu\text{m}$). In Fig. 3

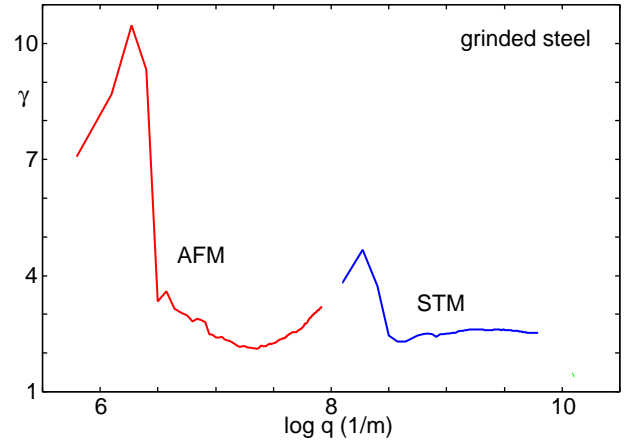


FIG. 4: The γ -parameter calculated from the AFM and the STM surface topography data shown in Fig. 2. The maximum of γ occur for $q \approx 1.8 \times 10^6 \text{ m}^{-1}$, corresponding to a wavelength $\lambda = 2\pi/q \approx 3.5 \mu\text{m}$. This is just the wavelength of surface topography orthogonal to the major wear tracks in Fig. 2.

I show the (angular averaged) surface roughness power spectrum $C(q)$ calculated from the AFM and the STM surface topography data shown in Fig. 2. The power spectrum is well approximated with self affine fractal with the fractal dimension $D_f = 2.25$. However, note that the surface topography is anisotropic. In Fig. 4 we show the calculated (using (19)) γ -parameter for the same surface. The maximum of γ occur for $q \approx 1.8 \times 10^6 \text{ m}^{-1}$, corresponding to a wavelength $\lambda = 2\pi/q \approx 3.5 \mu\text{m}$. This is just the wavelength of the surface topography orthogonal to the major wear tracks in Fig. 2.

In Fig. 5 we show the calculated (using (19)) γ -parameter for a sandblasted PMMA surface. In this case the statistical properties of the surface are expected to be isotropic, and indeed γ is very close to unity.

For surfaces which have been grinded or polished in one direction, wear scars may occur almost uninterrupted for a very long distance. In this case it is necessary to measure the surface topography over a very large surface area in order to correctly obtain the $\gamma(\zeta)$ -function. In numerical flow calculations as involved in, e.g., the studies of Patir and Cheng, it would be necessary to use very large rectangular units which would be practically impossible because of the huge memory and computational time required.

5. Contact mechanics: short review and basic equations

At short (average) interfacial separation there will be a direct asperity interaction between the solids walls, and in this case the perturbation approach of Sec. 2 will fail. Here we will briefly review the contact mechanics model of Persson which we use in this study.

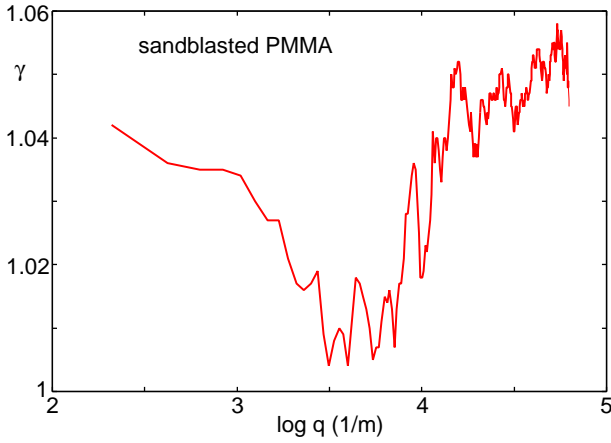


FIG. 5: The γ -parameter calculated from optically measured surface topography data for sandblasted PMMA. The surface topography was measured over a $3 \text{ cm} \times 3 \text{ cm}$ surface area. The surface root-mean-square roughness was $32 \mu\text{m}$.

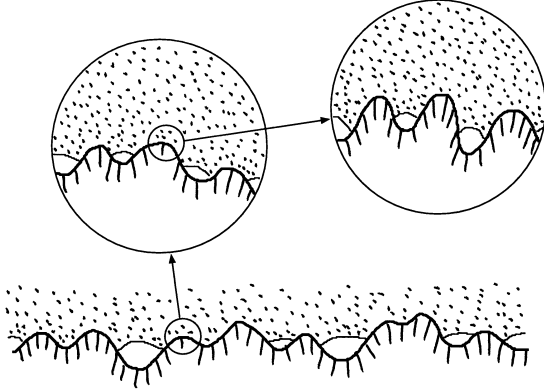


FIG. 6: An rubber block (dotted area) in adhesive contact with a hard rough substrate (dashed area). The substrate has roughness on many different length scales and the rubber makes partial contact with the substrate on all length scales. When a contact area is studied at low magnification it appears as if complete contact occur, but when the magnification is increased it is observed that in reality only partial contact occur.

Consider the frictionless contact between two elastic solids with the Young's elastic modulus E_0 and E_1 and the Poisson ratios ν_0 and ν_1 . Assume that the solid surfaces have the height profiles $h_0(\mathbf{x})$ and $h_1(\mathbf{x})$, respectively. The elastic contact mechanics for the solids is equivalent to those of a rigid substrate with the height profile $h(\mathbf{x}) = h_0(\mathbf{x}) + h_1(\mathbf{x})$ and a second elastic solid with a flat surface and with the Young's modulus E and the Poisson ratio ν chosen so that[15]

$$\frac{1 - \nu^2}{E} = \frac{1 - \nu_0^2}{E_0} + \frac{1 - \nu_1^2}{E_1}.$$

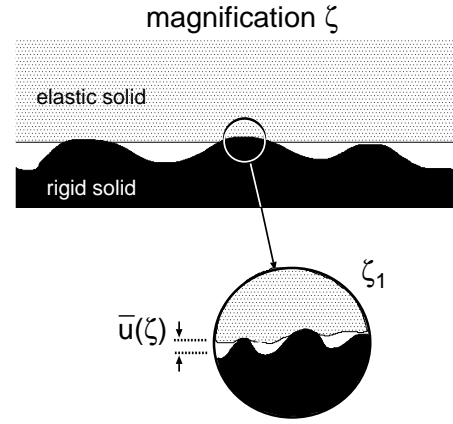


FIG. 7: An asperity contact region observed at the magnification ζ . It appears that complete contact occur in the asperity contact region, but when the magnification is increasing to the highest (atomic scale) magnification ζ_1 , it is observed that the solids are actually separated by the average distance $\bar{u}(\zeta)$.

The contact mechanics formalism developed elsewhere[7, 8, 13, 14] is based on the studying the interface between two contacting solids at different magnification ζ . When the system is studied at the magnification ζ it appears as if the contact area (projected on the xy -plane) equals $A(\zeta)$, but when the magnification increases it is observed that the contact is incomplete (see Fig. 6), and the surfaces in the apparent contact area $A(\zeta)$ are in fact separated by the average distance $\bar{u}(\zeta)$, see Fig. 7. The (apparent) relative contact area $A(\zeta)/A_0$ at the magnification ζ is given by[8, 13]

$$\frac{A(\zeta)}{A_0} = \frac{1}{(\pi G)^{1/2}} \int_0^{p_0} d\sigma e^{-\sigma^2/4G} = \text{erf}\left(\frac{p_0}{2G^{1/2}}\right) \quad (21)$$

where

$$G(\zeta) = \frac{\pi}{4} \left(\frac{E}{1 - \nu^2} \right)^2 \int_{q_0}^{\zeta q_0} dq q^3 C(q)$$

where the surface roughness power spectrum

$$C(q) = \frac{1}{(2\pi)^2} \int d^2x \langle h(\mathbf{x})h(\mathbf{0}) \rangle e^{-i\mathbf{q} \cdot \mathbf{x}}$$

where $\langle \dots \rangle$ stands for ensemble average. The height profile $h(\mathbf{x})$ of the rough surface can be measured routinely today on all relevant length scales using optical and stylus experiments.

The quantity $\bar{u}(\zeta)$ is the average separation between the surfaces in the apparent contact regions observed at the magnification ζ , see Fig. 7. It can be calculated from[8]

$$\begin{aligned} \bar{u}(\zeta) &= \sqrt{\pi} \int_{\zeta q_0}^{q_1} dq q^2 C(q) w(q, \zeta) \\ &\times \int_{p(\zeta)}^{\infty} dp' \frac{1}{p'} e^{-[w(q, \zeta)p'/E^*]^2}, \end{aligned}$$

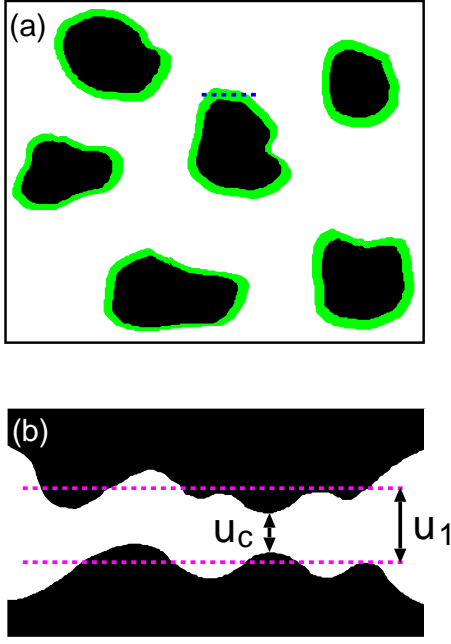


FIG. 8: (a) The black area is the asperity contact regions at the magnification ζ . The green area is the additional contact area observed when the magnification is reduced to $\zeta - \Delta\zeta$ (where $\Delta\zeta$ is small). The average separation between the solid walls in the green surface area is denoted by $u_1(\zeta)$. (b) The separation between the solid walls along the blue dashed line in (a). Since the surfaces of the solids are everywhere rough the actual separation between the solid walls in the green area will fluctuate around the average $u_1(\zeta)$. At the most narrow constriction the surface separation is u_c .

where $p(\zeta) = p_0 A_0 / A(\zeta)$ and

$$w(q, \zeta) = \left(\pi \int_{\zeta q_0}^q dq' q'^3 C(q') \right)^{-1/2}.$$

We define $u_1(\zeta)$ to be the (average) height separating the surfaces which appear to come into contact when the magnification decreases from ζ to $\zeta - \Delta\zeta$, where $\Delta\zeta$ is a small (infinitesimal) change in the magnification. In Fig. 8(a) the black area is the asperity contact regions at the magnification ζ . The green area is the additional contact area observed when the magnification is reduced to $\zeta - \Delta\zeta$ (where $\Delta\zeta$ is small)[16]. The average separation between the solid walls in the green surface area is given by $u_1(\zeta)$. Fig. 8(b) shows the separation between the solid walls along the dashed line in Fig. 8(a). Since the surfaces of the solids are everywhere rough the actual separation between the solid walls in the green area will fluctuate around the average $u_1(\zeta)$. Thus we expect the smallest surface separation $u_c = \alpha u_1(\zeta_c)$, where $\alpha < 1$ (but of order unity, see Fig. 8(b))[17]. In Ref. [12, 18] we have analyzed leak-rate data for rubber seals and always found that α to be in the range 0.5 – 1. However, it is clear that α cannot be a fixed constant but must depend on the

average surface separation and on the surface roughness which occur at length scales shorter than $\lambda = L/\zeta$. In particular, as $\langle h^2 \rangle_\zeta / u_1^2(\zeta) \rightarrow 0$ we expect that $\alpha \rightarrow 1$ (see also Sec. 8).

$u_1(\zeta)$ is a monotonically decreasing function of ζ , and can be calculated from the average interfacial separation $\bar{u}(\zeta)$ and $A(\zeta)$ using (see Ref. [8])

$$u_1(\zeta) = \bar{u}(\zeta) + \bar{u}'(\zeta) A(\zeta) / A'(\zeta).$$

One can show[12] from the equations above that as the applied squeezing pressure $p_0 \rightarrow 0$, for the magnifications most relevant for calculating fluid flow (e.g., the leak-rate of seals), $u_1 \rightarrow \bar{u}$.

We note that when solving for the fluid flow between macroscopic surfaces with roughness one may in a mean-field type of treatment write the local nominal pressure (i.e., the pressure locally averaged over surface area with linear dimension of order the wavelength λ_0 of the longest surface roughness component) as[19]

$$p(\mathbf{x}, t) = p_{\text{fluid}}(\mathbf{x}, t) + p_{\text{solid}}(\mathbf{x}, t)$$

where p_{fluid} and p_{solid} are locally averaged nominal fluid pressure and solid wall-wall contact pressure, respectively. The pressure p_{solid} can be related to the interfacial separation $\bar{u}(\mathbf{x}, t)$ as described in Ref. [7, 8]. In particular, for large enough average surface separation[7]

$$p_{\text{solid}} \approx \beta E^* e^{-\bar{u}/u_0}$$

where β and u_0 can be calculated from the surface roughness power spectrum.

6. Critical-junction theory of fluid flow

The perturbation expansion presented in Sec. 3 assumed no direct contact between the solid walls. But direct contact between the solid walls occur in most cases of interest, e.g., in static seals. The simplest approach for this case is based on the leak-rate model developed in Ref. [12, 20–24]. Consider the fluid leakage through a (nominal) contact region, say between a hard solid and rubber, from a high fluid pressure P_a region, to a low fluid pressure P_b region. Assume that the nominal contact region between the rubber and the hard countersurface is rectangular with area $L_x \times L_y$, with $L_y > L_x$. We assume that the high pressure fluid region is for $x < 0$ and the low pressure region for $x > L_x$. We “divide” the contact region into squares with the side $L_x = L$ and the area $A_0 = L^2$ (this assumes that $N = L_y/L_x$ is an integer, but this restriction does not affect the final result). Now, let us study the contact between the two solids within one of the squares as we change the magnification ζ . We define $\zeta = L/\lambda$, where λ is the resolution. We study how the apparent contact area (projected on the xy -plane), $A(\zeta)$, between the two solids depends on the magnification ζ . At the lowest magnification we cannot observe any surface roughness, and the contact between the solids appears to be complete i.e., $A(1) = A_0$. As we increase the

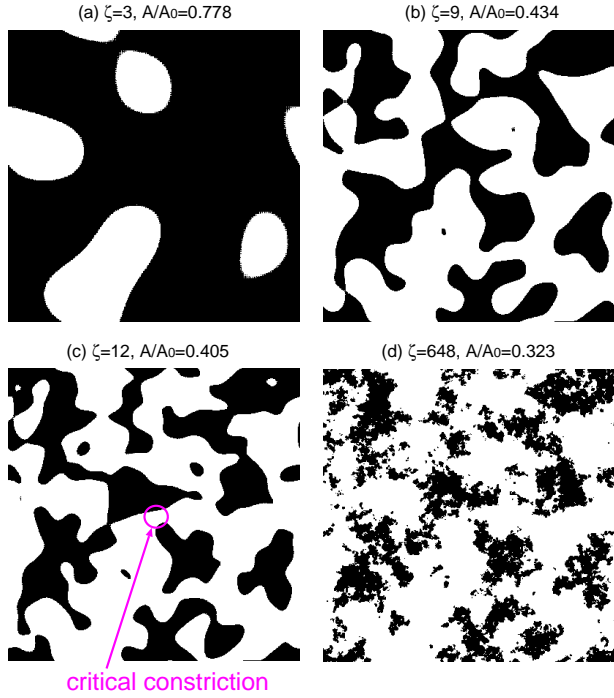


FIG. 9: The contact region at different magnifications $\zeta = 3, 9, 12$ and 648 , is shown in (a)-(d) respectively. When the magnification increases from 9 to 12 the non-contact region percolate. At the lowest magnification $\zeta = 1$: $A(1) = A_0$. The figure is the result of Molecular Dynamics simulations of the contact between elastic solids with randomly rough surfaces, see Ref. [22].

magnification we will observe some interfacial roughness, and the (apparent) contact area will decrease. At high enough magnification, say $\zeta = \zeta_c$, a percolating path of non-contact area will be observed for the first time, see Fig. 9. We denote the most narrow constriction along this percolation path as the *critical constriction*. The critical constriction will have the lateral size $\lambda_c = L/\zeta_c$ and the surface separation at this point is denoted by $u_c = \alpha u_1(\zeta_c)$. As we continue to increase the magnification we will find more percolating channels between the surfaces, but these will have more narrow constrictions than the first channel which appears at $\zeta = \zeta_c$, and as a first approximation one may neglect the contribution to the leak-rate from these channels[22].

A first rough estimate of the leak-rate is obtained by assuming that all the leakage occurs through the critical percolation channel, and that the whole pressure drop $\Delta P = P_a - P_b$ (where P_a and P_b is the pressure to the left and right of the seal) occurs over the critical constriction (of width and length $\lambda_c \approx L/\zeta_c$ and height u_c). We will refer to this theory as the “critical-junction” theory. If we approximate the critical constriction as a pore with rectangular cross section (width and length λ_c and height $u_c \ll \lambda_c$), and if we assume an incompressible Newtonian fluid, the volume-flow per unit time through

the critical constriction will be given by (Poiseuille flow)

$$\dot{Q} = \frac{u_c^3}{12\eta} \Delta P, \quad (22)$$

where η is the fluid viscosity. In deriving (22) we have assumed laminar flow and that $u_c \ll \lambda_c$, which is always satisfied in practice. We have also assumed no-slip boundary condition on the solid walls. This assumption is not always satisfied at the micro or nano-scale, but is likely to be a very good approximation in the present case owing to surface roughness which occurs at length-scales shorter than the size of the critical constriction. Finally, since there are $N = L_y/L_x$ square areas in the rubber-countersurface (apparent) contact area, we get the total leak-rate

$$\dot{Q} = \frac{L_y}{L_x} \frac{u_c^3}{12\eta} \Delta P. \quad (23)$$

Note that a given percolation channel could have several narrow (critical or nearly critical) constrictions of nearly the same dimension which would reduce the flow along the channel. But in this case one would also expect more channels from the high to the low fluid pressure side of the junction, which would tend to increase the leak rate. These two effects will, at least in the simplest picture where one assumes that the distance between the critical junctions along a percolation path (in the x -direction) is the same as the distance between the percolation channels (in the y -direction), compensate each other (see Ref. [22]). The effective medium theory presented below includes (in an approximate way) all the flow channels.

To complete the theory we must calculate the separation u_c of the surfaces at the critical constriction. We first determine the critical magnification ζ_c by assuming that the apparent relative contact area at this point is given by percolation theory. Thus, the relative contact area $A(\zeta)/A_0 \approx 1 - p_c$, where p_c is the so called percolation threshold[25]. For infinite-sized 2D systems, and assuming site percolation, $p_c \approx 0.70$ for a hexagonal lattice, 0.59 for a square lattice, and 0.5 for a triangular lattice[25]. For bond percolation the corresponding numbers are $0.65, 0.5$, and 0.35 , respectively. For continuous percolation in 2D the Bruggeman effective medium theory predict $p_c = 0.5$. For finite sized systems the percolation will, on the average, occur for (slightly) smaller values of p_c , and fluctuations in the percolation threshold will occur between different realizations of the same physical system. Numerical simulations such as those presented in Ref. [22] (see Fig. 9) and Ref. [26] typically gives p_c slightly larger than 0.5 . In our earlier leak-rate studies we have used $p_c = 0.5$ and 0.6 to determine the critical magnification $\zeta = \zeta_c$.

We can write the leak-rate in terms of the pressure flow factor. Thus the current

$$J_x = -\frac{\bar{u}^3 \phi_p}{12\eta} \frac{dp}{dx} = -\frac{\bar{u}^3 \phi_p}{12\eta} \frac{\Delta P}{L_x}$$

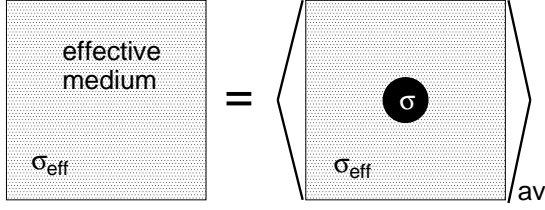


FIG. 10: Effective medium theories take into account random disorder in a physical system, e.g., random fluctuations in the interfacial separation $u(\mathbf{x})$. Thus, for a n -component system (e.g., where the separation u takes n different discrete values) the flow in the effective medium should be the same as the average fluid flow obtained when circular regions of the n -components are embedded in the effective medium. Thus, for example, the pressure p at the origin calculated assuming that the effective medium occur everywhere must equal the average $\sum c_i p_i$ (where c_i is the concentration of component i) of the pressures p_i (at the origin) calculated with the circular inclusion of component $i = 1, \dots, n$.

and the leak-rate

$$\dot{Q} = J_x L_y = \frac{L_y}{L_x} \frac{\bar{u}^3 \phi_p}{12\eta} \Delta P$$

Comparing this with (23) gives

$$\phi_p = \left(\frac{u_c}{\bar{u}}\right)^3 = \left(\alpha \frac{u_1(\zeta_c)}{\bar{u}(1)}\right)^3$$

7. Effective medium theory of fluid flow: isotropic roughness

The critical-junction theory presented above assumes that the leak-rate is determined by the resistance towards fluid flow through the critical constriction (or through a network of critical constrictions, see above). In reality there will be many flow channels at the interface. Here we will use the 2D Bruggeman effective medium theory[27, 28] to calculate (approximately) the leak-rate resulting from the network of flow channels. Another approach to extend the critical junction theory is critical path analysis, see Ref. [29, 30].

We study the fluid flow through an interface where the separation $u(\mathbf{x})$ between the surfaces varies with the lateral coordinate $\mathbf{x} = (x, y)$. If $u(\mathbf{x})$ varies slowly with \mathbf{x} the Navier-Stokes equations of fluid flow reduces to

$$\mathbf{J} = -\sigma \nabla p \quad (24)$$

where the conductivity $\sigma = u^3(\mathbf{x})/12\eta$.

In the effective medium approach one replace the local, spatial varying, conductivity $\sigma(\mathbf{x})$ with a constant effective conductivity σ_{eff} . Thus the fluid flow current equation

$$\mathbf{J} = -\sigma_{\text{eff}} \nabla p, \quad (25)$$

as applied to a rectangular region $L_x \times L_y$ with the pressure gradient $dp/dx = (P_b - P_a)/L_x$, gives

$$\dot{Q} = L_y J_x = \frac{L_y}{L_x} \sigma_{\text{eff}} \Delta P \quad (26)$$

where $\Delta P = P_a - P_b$ is the pressure drop.

The effective medium conductivity σ_{eff} is obtained as follows. Let us study the current flow at a circular inclusion (radius R) with the (constant) conductivity σ located in an infinite conducting sheet with the (constant) conductivity σ_{eff} . We introduce polar coordinates with the origin at the center of the circular inclusion. The current

$$\mathbf{J} = -\sigma \nabla p \quad \text{for} \quad r < R$$

$$\mathbf{J} = -\sigma_{\text{eff}} \nabla p \quad \text{for} \quad r > R$$

We consider a steady state so that

$$\nabla \cdot \mathbf{J} = 0$$

or

$$\nabla^2 p = 0 \quad (27)$$

If $\mathbf{J}_0 = -\sigma_{\text{eff}} \mathbf{a}$ is the current far from the inclusion (assumed to be constant) we get for $r > R$:

$$p = [1 + f(r)] \mathbf{a} \cdot \mathbf{x} \quad (28)$$

Eq. (27) is satisfied if

$$f''(r) + 3f'(r)r^{-1} = 0$$

A solution to this equation is $f = \alpha r^{-2}$. Substituting this in (28) gives

$$p = [1 + \alpha r^{-2}] \mathbf{a} \cdot \mathbf{x} \quad (29)$$

For $r < R$ we have the solution

$$p = \beta \mathbf{a} \cdot \mathbf{x} \quad (30)$$

Since p and $\mathbf{x} \cdot \mathbf{J}$ must be continuous at $r = R$ we get from (28) and (29):

$$1 + \alpha R^{-2} = \beta$$

$$(1 - \alpha R^{-2}) \sigma_{\text{eff}} = \beta \sigma$$

Combining these two equations gives

$$\beta = \frac{2\sigma_{\text{eff}}}{\sigma_{\text{eff}} + \sigma} \quad (31)$$

The basic picture behind effective medium theories is presented in Fig. 10. Thus, for a two component system, one assumes that the flow in the effective medium should

be the same as the average fluid flow obtained when circular regions of the two components are embedded in the effective medium. Thus, for example, the pressure p calculated assuming that the effective medium occur everywhere must equal the average $c_1 p_1 + c_2 p_2$ of the pressures p_1 and p_2 calculated with the circular inclusion of the two components **1** and **2**, respectively. For $r < R$ we have for the effective medium $p = \mathbf{a} \cdot \mathbf{x}$ and using (30) the equation $p = c_1 p_1 + c_2 p_2$ gives

$$1 = c_1 \beta_1 + c_2 \beta_2 \quad (32)$$

where c_1 and c_2 are the fractions of the total area occupied by the components **1** and **2**, respectively. Using (31) and (32) gives

$$1 = c_1 \frac{2\sigma_{\text{eff}}}{\sigma_{\text{eff}} + \sigma_1} + c_2 \frac{2\sigma_{\text{eff}}}{\sigma_{\text{eff}} + \sigma_2}$$

which is the standard Bruggeman effective medium for a two component system. Note that if one component is insulating, say $\sigma_2 = 0$, as $c_1 \rightarrow 0.5$ from above, $\sigma_{\text{eff}} \rightarrow 0$, i.e., $p_c = 1/2$ is the percolation threshold of the two component 2D-Bruggeman effective medium model.

If one instead have a continuous distribution of components (which we number by the continuous index ξ) with conductivities $\sigma = \sigma(\xi)$, then

$$1 = \int d\xi P(\xi) \beta(\xi) \quad (33)$$

where $P(\xi)$ is the fraction of the total surface area occupied by the component denoted by ξ . The probability distribution $P(\xi)$ is normalized so that

$$\int d\xi P(\xi) = 1 \quad (34)$$

Using (31) we get

$$1 = \int d\xi P(\xi) \frac{2\sigma_{\text{eff}}}{\sigma_{\text{eff}} + \sigma(\xi)} \quad (35)$$

It is easy to show from this equation that also for the case of a continuous distribution of components, the percolation limit occur when the non-conducting component (which in our case correspond to the area of real contact where $u = 0$ and hence $\sigma = u^3/12\eta = 0$) occupies 50% of the total surface area, i.e., $p_c = 1/2$ in this case too.

To summarize, using the 2D Bruggeman effective medium theory we get:

$$\dot{Q} = \frac{L_y}{L_x} \sigma_{\text{eff}} \Delta P, \quad (36)$$

where $\Delta P = P_a - P_b$ is the pressure drop and where

$$\frac{1}{\sigma_{\text{eff}}} = \int d\sigma P(\sigma) \frac{2}{\sigma_{\text{eff}} + \sigma}$$

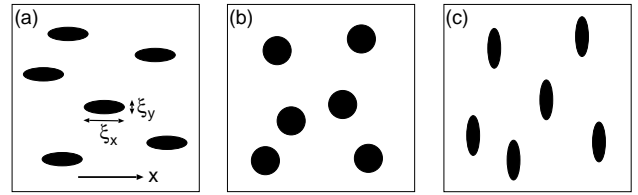


FIG. 11: Contact regions for (a) longitudinal oriented, (b) isotropic, and (c) transversely oriented rough surfaces. The ratio between the ellipse major axis is denoted by $\gamma = \xi_x/\xi_y$ and $\gamma > 1$, $= 1$ and < 1 in (a), (b) and (c), respectively. The average fluid flow is in the x -direction.

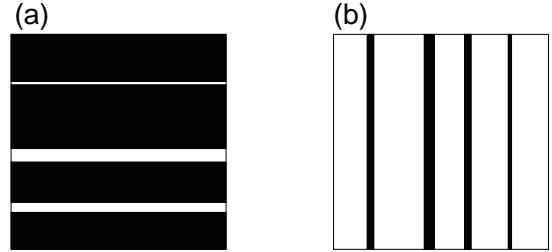


FIG. 12: The black area denote interfacial solid-solid contact with the flow conductivity $\sigma_2 = 0$. The two cases (a) and (b) correspond to $\gamma = \infty$ and $\gamma = 0$, respectively. In the first case (a) fluid flow can occur in the strips (open channels) of component 1 for arbitrary low concentration of component 1. In this case fluid flow will occur at the interface until complete contact occur between the solids. In the opposite limit $\gamma \rightarrow 0$ no fluid can flow (in the x -direction) at the interface unless c_2 is zero.

$$= \int d\zeta \left(-\frac{A'(\zeta)}{A_0} \right) \frac{2}{\sigma_{\text{eff}} + \sigma(\zeta)}, \quad (37)$$

where

$$\sigma(\zeta) = \frac{[\alpha u_1(\zeta)]^3}{12\eta}. \quad (38)$$

Eq. (37) is easy to solve by iteration.

8. Effective medium theory of fluid flow: anisotropic roughness

Here we briefly describe how one may apply the effective medium theory to study fluid flow between surfaces with anisotropic (but translational invariant) statistical properties. Let p be the locally averages pressure and \mathbf{J} the fluid flow current also locally averaged. We have

$$J_i = -\sigma_{ij}^{\text{eff}} \frac{\partial p}{\partial x_j} \quad (39)$$

Note that

$$\sigma_{ij}^{\text{eff}} = \frac{\bar{u}^3}{12\eta} (\phi_p)_{ij}.$$

We can choose a coordinate system such that the flow conductivity tensor is diagonal:

$$\sigma_{\text{eff}} = \begin{pmatrix} \sigma_{\parallel} & 0 \\ 0 & \sigma_{\perp} \end{pmatrix}$$

In this case the x and y -coordinate axis are oriented along and perpendicular to the “groves” on the surface, respectively. The flow conductivity for any other orientation can be obtained using the standard transformation of tensors under rotation. Thus if the x axis is oriented at an angle ϕ relative to the “groves” then

$$\sigma_{\text{eff}} = \begin{pmatrix} \sigma_{\parallel} \cos^2 \phi + \sigma_{\perp} \sin^2 \phi & (\sigma_{\parallel} - \sigma_{\perp}) \cos \phi \sin \phi \\ (\sigma_{\parallel} - \sigma_{\perp}) \cos \phi \sin \phi & \sigma_{\parallel} \sin^2 \phi + \sigma_{\perp} \cos^2 \phi \end{pmatrix}$$

We will now calculate the flow conductivities σ_{\parallel} and σ_{\perp} parallel and perpendicular to the groves, respectively. We assume that interfacial separation $u(\mathbf{x})$ varies slowly with $\mathbf{x} = (x, y)$. Consider an elliptic inclusion in a fluid. Assume that the fluid flow conductivity equals σ_{eff} outside the inclusion and σ_1 in the inclusion. Assume that the fluid flow far from the inclusion is oriented at an angle ϕ relative to a major axis of the inclusion, i.e., far from the inclusion $\mathbf{J} = -\sigma_{\text{eff}} \mathbf{a}$ and

$$p = \mathbf{a} \cdot \mathbf{x} = a(x \cos \phi + y \sin \phi) \quad (40)$$

The fluid flow can be calculated analytically using elliptic coordinates (μ, ϑ) , see Ref. [31]. In this coordinate system the curves $\mu = \text{const.}$ are ellipses. Consider the ellipse $\mu = \mu_0$. The ratio γ between the major and minor axis can be written as $\gamma = \coth \mu_0$ so that when $\mu_0 \rightarrow \infty$ the ellipse becomes a circle.

The fluid pressure inside the elliptic inclusion is given by

$$p = A_{ij} a_i x_j \quad (41)$$

where the matrix A_{ij} has the components $A_{12} = A_{21} = 0$ and

$$A_{11} = \frac{\sigma_{\text{eff}} e^{\mu_0}}{\sigma_{\text{eff}} \cosh \mu_0 + \sigma_1 \sinh \mu_0} \quad (42)$$

$$A_{22} = \frac{\sigma_{\text{eff}} e^{\mu_0}}{\sigma_1 \cosh \mu_0 + \sigma_{\text{eff}} \sinh \mu_0} \quad (43)$$

Note that when $\mu_0 \rightarrow \infty$ the matrix $A_{ij} = \beta \delta_{ij}$, where β is given by (A8). Thus in this case the pressure in the inclusion becomes $p = \beta \mathbf{a} \cdot \mathbf{x}$ just as for a circular inclusion (see Eq. (A7)), which of course is expected because the ellipse becomes a circle when $\mu_0 \rightarrow \infty$.

The parameter μ_0 is determined by $\gamma = \coth \mu_0$ or

$$e^{2\mu_0} = \frac{\gamma + 1}{\gamma - 1}$$

Using this equation we can also write (42) and (43) as

$$A_{11} = \frac{\sigma_{\text{eff}}(\gamma + 1)}{\sigma_{\text{eff}}\gamma + \sigma_1} \quad (44)$$

$$A_{22} = \frac{\sigma_{\text{eff}}(\gamma + 1)}{\sigma_1\gamma + \sigma_{\text{eff}}} \quad (45)$$

We now consider the situation where $\phi = 0$ so that one of the ellipse axis is oriented along the (average) fluid flow direction as in Fig. 11(a). In this case the pressure in the inclusion

$$p = A_{11} ax$$

while the pressure far away from the inclusion $p = ax$. For a two-component system the effective medium equation (33) now becomes

$$1 = \frac{c_1 \sigma_{\text{eff}}(\gamma_1 + 1)}{\sigma_{\text{eff}}\gamma_1 + \sigma_1} + \frac{c_2 \sigma_{\text{eff}}(\gamma_2 + 1)}{\sigma_{\text{eff}}\gamma_2 + \sigma_2} \quad (46)$$

where we have taken into account that the two components may have different ratio γ . Assume that one component, say component 2, has the conductivity $\sigma_2 = 0$. In this case it follows from (46) that $\sigma_{\text{eff}} \rightarrow 0$ as $c_2 \rightarrow \gamma_1/(\gamma_1 + 1)$. Note in particular that for $\gamma_1 \rightarrow \infty$, $c_2 \rightarrow 1$ i.e. in the limit when the major axis of the inclusion 1 goes to infinite (where conducting strips of the conducting component 1 occur for arbitrary low concentration of component 1) fluid flow will occur at the interface until complete contact occur between the solids. In the opposite limit $\gamma_1 \rightarrow 0$, $c_2 \rightarrow 0$. In this case no fluid can flow (in the x -direction) at the interface for any applied pressure. These two limits correspond to the configurations illustrated in Fig. 12.

For a continuous distribution of components

$$1 = \int d\zeta P(\zeta) \frac{\sigma_{\text{eff}}(\gamma(\zeta) + 1)}{\sigma_{\text{eff}}\gamma(\zeta) + \sigma(\zeta)} \quad (47)$$

where $\sigma(\zeta) = (\alpha u_1(\zeta))^3/12\eta$. This equation is also valid for the orientation of the ellipse as in Fig. 11(c) in which case $\gamma < 1$ (in general, γ is the ratio between the ellipse axis in the x -direction and the y -direction).

In Fig. 13 we show the pressure flow factor ϕ_p as a function of the average surface separation \bar{u} in units of the root-mean-square roughness amplitude. In the calculation we have for simplicity assumed that $\gamma(\zeta)$ is a constant independent of the magnification ζ . Results are shown for three different surfaces with surface roughness with isotropic statistical properties ($\gamma = 1$), and for surfaces with anisotropic roughness of longitudinal ($\gamma = 3$) and transverse ($\gamma = 1/3$) type. The dashed lines is calculated with $\alpha = 1$ while the solid lines is calculated with a α which depends on the interfacial separation as follows:

As pointed out in Sec. 5, the surfaces in the (non-contact) flow channels are everywhere rough, and the actual separation between the solid walls in the non-contact region which appears when the magnification is reduced from ζ to $\zeta - \Delta\zeta$ (green area in Fig. 8(a)) will fluctuate around the average $u_1(\zeta)$. Thus with respect to fluid flow the separation u between the walls will appear smaller than the average u_1 and we use $u = \alpha u_1(\zeta)$,

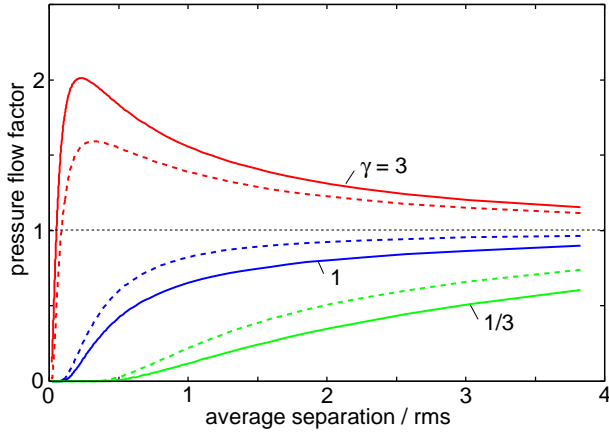


FIG. 13: The pressure flow factor ϕ_p as a function of the average surface separation \bar{u} in units of the root-mean-square roughness amplitude. For three different surfaces with surface roughness with isotropic statistical properties ($\gamma = 1$), and for surfaces with anisotropic roughness of longitudinal ($\gamma = 3$) and transverse ($\gamma = 1/3$) type. The $\gamma = 1$ case is for sandblasted PMMA (root-mean-square roughness $22 \mu\text{m}$) in contact with rubber with the elastic modulus $E = 2.3 \text{ MPa}$. The other cases assumes the same angular averaged power spectrum and elastic properties as for the $\gamma = 1$ case. The solid and dashed lines are discussed in the text.

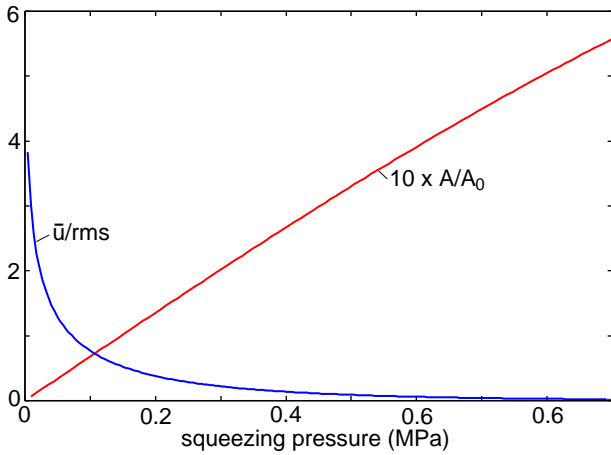


FIG. 14: The variation of the area of real contact A (in units of the nominal contact area A_0) and the average interfacial separation \bar{u} (in units of the root-mean-square roughness amplitude) as a function of the (nominal) squeezing pressure for the system shown in Fig. 13: sandblasted PMMA (root-mean-square roughness $22 \mu\text{m}$) in contact with rubber with the elastic modulus $E = 2.3 \text{ MPa}$.

where $\alpha < 1$. We note that α is due to the surface roughness which occur at length scales *shorter* than $\lambda = L/\zeta$, and it is possible to calculate (or estimate) α from the surface roughness power spectrum, as follows.

As shown in Sec. 2 and Appendix A, the fluid flow between two nominal flat surfaces is affected by the surface roughness on the solid walls even at such large (average) surface separation that no direct wall-wall contact occur.

Thus for isotropic roughness at large separation there is a reduction in the fluid flow entering via the flow factor $\phi_p \approx 1 - (3/2)(\langle h^2 \rangle / u^2)$, where u is the average surface separation. If we apply this to the present case in the fluid flow problem we replace the term $u_1^3(\zeta)$ by $u_1^3(\zeta)\phi_p^*$ where

$$\phi_p^* = \left(1 + \frac{3}{2} \frac{\langle h^2 \rangle_{\zeta^*}}{u_1^2(\zeta^*)}\right)^{-1}$$

Here we have assumed surface roughness with isotropic statistical properties and $\langle h^2 \rangle_{\zeta}$ denote the ensemble average of the square of the roughness amplitude including only the surface roughness with wavevectors larger than $q = \zeta^* q_0$. In calculating the solid lines in Fig. 13 we have chosen $\zeta^* = 3\zeta$.

Fig. 13 shows, as expected, that when γ decreases the percolation limit, below which no fluid flow can occur, appears at larger and larger average separation. Note also that for $\gamma = 3$ the pressure flow factor first increases with decreasing \bar{u} , but finally it decreases towards zero. Thus, even for arbitrary large γ at high enough squeezing pressures (corresponding to small enough \bar{u}) the non-contact area will not percolate in which case no fluid flow can occur at the interface and $\phi_p = 0$.

Fig. 14 shows the variation of the area of real contact A (in units of the nominal contact area A_0) and the average interfacial separation \bar{u} (in units of the root-mean-square roughness amplitude) as a function of the (nominal) squeezing pressure for the system shown in Fig. 13: sandblasted PMMA (root-mean-square roughness $22 \mu\text{m}$) in contact with rubber with the elastic modulus $E = 2.3 \text{ MPa}$. Note that even at the lowest squeezing pressure where $\bar{u}/rms \approx 4$ the area of real contact is still non-negligible, about 1% of the nominal contact area.

9. Summary and conclusion

I have studied the fluid flow at the interface between elastic solids with randomly rough surfaces. I have used the contact mechanics model of Persson to take into account the elastic interaction between the solid walls and the Bruggeman effective medium theory to account for the influence of the disorder on the fluid flow. I have calculate the flow tensor which determines the pressure flow factor and, e.g., the leak-rate of seals. I have shown how the perturbation treatment of Tripp can be extended to arbitrary order in the ratio between the root-mean-square roughness amplitude and the average interfacial surface separation. I have introduced a matrix $D(\zeta)$, determined by the surface roughness power spectrum, which can be used to describe the anisotropy of the surface at any magnification ζ . I have present results for the asymmetry factor $\gamma(\zeta)$ (generalized Peklenik number) for a grinded steel surface and a sandblasted PMMA surface.

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Appendix A

In Sec. 2 we calculated the pressure and shear flow factors to first order in $\langle h^2 \rangle / \bar{u}^2$. Here we will present a simpler and more powerful approach, which is in the spirit of the Renormalization Group (RG) procedure. Thus we will eliminate or integrate out the surface roughness components in steps and obtain a set of RG flow equations describing how the effective fluid equation evolves as more and more of the surface roughness components are eliminated.

Assume that after eliminating all the surface roughness components with wavevector $|\mathbf{q}| = q > \zeta q_0$ the fluid current [given by (1)] takes the form

$$\mathbf{J} = -\frac{1}{12\eta} A(u) \nabla p + \frac{1}{2} B(u) \mathbf{v} \quad (\text{A1})$$

where A and B are 2×2 matrices. We now add to u a small amount of roughness

$$h = \int_{(\zeta - \Delta\zeta)q_0 < q < \zeta q_0} d^2 q h(\mathbf{q}) e^{i\mathbf{q} \cdot \mathbf{x}} \quad (\text{A2})$$

Consider now the current

$$\mathbf{J} = -\frac{1}{12\eta} A(u+h) \nabla p + \frac{1}{2} B(u+h) \mathbf{v}$$

Writing as before

$$p = p_0 + p_1 + p_2$$

we get to second order in h

$$\begin{aligned} \mathbf{J} = & -\frac{A(u)}{12\eta} \nabla(p_0 + p_1 + p_2) \\ & -\frac{A'(u)h}{12\eta} \nabla(p_0 + p_1) - \frac{A''(u)h^2}{24\eta} \nabla p_0 \\ & + \frac{1}{2} (B(u) + B'(u)h) \mathbf{v} + \frac{1}{4} B''(u)h^2 \mathbf{v} \end{aligned} \quad (\text{A3})$$

The ensemble average of this current gives to second order in h

$$\begin{aligned} \langle \mathbf{J} \rangle = & -\frac{A(u)}{12\eta} \nabla \bar{p} \\ & -\frac{A'(u)}{12\eta} \langle h \nabla p_1 \rangle - \frac{A''(u) \langle h^2 \rangle}{24\eta} \nabla \bar{p} \end{aligned}$$

$$+\frac{1}{2} B(u) \mathbf{v} + \frac{1}{4} B''(u) \langle h^2 \rangle \mathbf{v} \quad (\text{A4})$$

where we have used that $\langle h \rangle = 0$. To zero order in h the continuity equation $\nabla \cdot \mathbf{J}$ gives

$$A_{ij}(u) \partial_i \partial_j p_0 = 0,$$

and to first order in h we get

$$-\frac{A'_{ij}(u)}{12\eta} \partial_i h \partial_j p_0 - \frac{A_{ij}(u)}{12\eta} \partial_i \partial_j p_1 + \frac{1}{2} B'_{ij}(u) \partial_i h v_j = 0$$

In wavevector space this equation takes the form

$$\begin{aligned} & -\frac{1}{12\eta} A'_{ij}(u) (iq_i) h(\mathbf{q}) \partial_j p_0 + \frac{1}{12\eta} A_{ij}(u) q_i q_j p_1(\mathbf{q}) \\ & + \frac{1}{2} B'_{ij}(u) (iq_i) h(\mathbf{q}) v_j = 0 \end{aligned}$$

or

$$\begin{aligned} p_1(\mathbf{q}) = & (A_{lm}(u) q_l q_m)^{-1} (iq_i) h(\mathbf{q}) \\ & \times (A'_{ij}(u) \partial_j p_0 - 6\eta B'_{ij}(u) v_j) \end{aligned} \quad (\text{A5})$$

Using this equation and (A2) gives

$$\begin{aligned} \langle h \partial_i p_1 \rangle = & \int d^2 q d^2 q' \langle h(\mathbf{q}') (iq_i) p_1(\mathbf{q}) \rangle \\ = & \int d^2 q C(q) (A_{lm}(u) q_l q_m)^{-1} q_i q_j \\ & \times (6\eta B'_{jk}(u) v_k - A'_{jk}(u) \partial_k p_0) \end{aligned} \quad (\text{A6})$$

Let us define the matrix

$$M_{ij} = \langle h^2 \rangle^{-1} \int d^2 q C(q) (A_{lm}(u) q_l q_m)^{-1} q_i q_j \quad (\text{A7})$$

so that (A5) becomes

$$\langle h \nabla p_1 \rangle = 6\eta M B' \mathbf{v} - M A' \nabla p_0$$

Substituting this in (A4) gives

$$\begin{aligned} \langle \mathbf{J} \rangle = & -\frac{1}{12\eta} \left(A(u) + \frac{1}{2} \langle h^2 \rangle A''(u) - \langle h^2 \rangle M A' \right) \nabla \bar{p} \\ & + \frac{1}{2} \left(B(u) + \frac{1}{2} \langle h^2 \rangle B''(u) - \langle h^2 \rangle M B'(u) \right) \mathbf{v} \end{aligned} \quad (\text{A8})$$

Note that this equation has the same general form as the original equation (A1). If we denote the matrices A and B in the original equation (A1) as $A(u, \zeta)$ and $B(u, \zeta)$ to indicate that these were the matrices obtained after eliminating all wavevector components of h

with $q > \zeta q_0$, then the new matrices obtained by eliminating the additional roughness with wavevectors between $(\zeta - \Delta\zeta)q_0 < q < \zeta q_0$ becomes

$$A(u, \zeta - \Delta\zeta) = A(u, \zeta) + \frac{1}{2}\langle h^2 \rangle A''(u, \zeta) - \langle h^2 \rangle A'(u, \zeta) M A'(u, \zeta) \quad (A9)$$

$$B(u, \zeta - \Delta\zeta) = B(u, \zeta) + \frac{1}{2}\langle h^2 \rangle B''(u, \zeta) - \langle h^2 \rangle A'(u, \zeta) M B'(u, \zeta) \quad (A10)$$

Since $\Delta\zeta$ is small we can expand the left hand side to linear order in $\Delta\zeta$. Furthermore note that

$$\begin{aligned} \frac{\langle h^2 \rangle}{\Delta\zeta} &= \frac{1}{\Delta\zeta} \int_{(\zeta - \Delta\zeta)q_0 < q < \zeta q_0} d^2q C(\mathbf{q}) \\ &= \frac{1}{\Delta\zeta} \int_{(\zeta - \Delta\zeta)q_0}^{\zeta q_0} dq q \int_0^{2\pi} d\phi C(q \cos\phi, q \sin\phi) \\ &= \zeta q_0^2 \int_0^{2\pi} d\phi C(\zeta q_0 \cos\phi, \zeta q_0 \sin\phi) \\ &= -\frac{d}{d\zeta} \int_{q > q_0 \zeta} d^2q C(\mathbf{q}) = -\frac{d}{d\zeta} \langle h^2 \rangle_\zeta \end{aligned} \quad (A11)$$

where $\langle h^2 \rangle_\zeta$ is the ensemble averaged of the square of the roughness amplitude including only roughness with wavevector $|\mathbf{q}| > \zeta q_0$. Thus from (A9), (A10) and (A11) we get

$$\frac{\partial A}{\partial \zeta} = \left[\frac{1}{2} A''(u, \zeta) - A'(u, \zeta) M A'(u, \zeta) \right] \frac{d}{d\zeta} \langle h^2 \rangle_\zeta \quad (A12)$$

$$\frac{\partial B}{\partial \zeta} = \left[\frac{1}{2} B''(u, \zeta) - A'(u, \zeta) M B'(u, \zeta) \right] \frac{d}{d\zeta} \langle h^2 \rangle_\zeta \quad (A13)$$

If we assume that $D(\zeta)$ is independent of ζ , it is easy to solve these equations using perturbation theory to arbitrary order in the surface roughness amplitude h . Since $A \rightarrow u^3$ and $\langle h^2 \rangle_\zeta \rightarrow 0$ as $\zeta \rightarrow \zeta_1$ we can write

$$A(u, \zeta) = u^3 + a_1(u) \langle h^2 \rangle_\zeta + a_2(u) \langle h^2 \rangle_\zeta^2 + \dots \quad (A14)$$

To first order in $\langle h^2 \rangle_\zeta$ we get from (A12)

$$a_1 = 3u - 9Mu^4$$

where

$$M = \frac{\int_{(\zeta - \Delta\zeta)q_0 < q < \zeta q_0} d^2q C(\mathbf{q}) u^{-3} q^{-2} \mathbf{q} \mathbf{q}}{\int_{(\zeta - \Delta\zeta)q_0 < q < \zeta q_0} d^2q C(\mathbf{q})}$$

or

$$M = u^{-3} \frac{\int_0^{2\pi} d\phi C(\mathbf{q}) q^{-2} \mathbf{q} \mathbf{q}}{\int_0^{2\pi} d\phi C(\mathbf{q})} = u^{-3} D(\zeta) \quad (A15)$$

where $|\mathbf{q}| = \zeta q_0$. Thus to first order in $\langle h^2 \rangle_\zeta$:

$$\begin{aligned} A(u, \zeta) &= u^3 + \langle h^2 \rangle_\zeta u^3 (1 - 3D) \\ &= u^3 \left(1 + \frac{\langle h^2 \rangle_\zeta}{u^2} 3(1 - 3D) \right) \end{aligned} \quad (A16)$$

Since $B \rightarrow u$ and $\langle h^2 \rangle_\zeta \rightarrow 0$ as $\zeta \rightarrow \zeta_1$ we can write

$$B(u, \zeta) = u + b_1(u) \langle h^2 \rangle_\zeta + b_2(u) \langle h^2 \rangle_\zeta^2 + \dots \quad (A17)$$

Substituting this in (A13) gives

$$b_1 = -3Mu^2.$$

Thus to first order in $\langle h^2 \rangle_\zeta$ we get

$$B(u, \zeta) = u - \langle h^2 \rangle_\zeta u^{-1} 3D = u \left(1 - \frac{\langle h^2 \rangle_\zeta}{u^2} 3D \right) \quad (A18)$$

It is strait forward to calculate the higher order terms (e.g., a_2 and b_2) in the expansions (A14) and (A17) but here we will only do so for the case of surface roughness with isotropic statistical properties. In this case $A_{ij} = A(u, \zeta) \delta_{ij}$ and $B_{ij} = B(u, \zeta) \delta_{ij}$. Thus the matrix M in (A7) becomes

$$M_{ij} = A^{-1} \langle h^2 \rangle^{-1} \int d^2q C(\mathbf{q}) q^{-2} q_i q_j = \frac{1}{2} A^{-1} \delta_{ij}$$

and (A12) and (A13) reduces to

$$\frac{\partial A}{\partial \zeta} = \frac{1}{2} \left[A''(u, \zeta) - \frac{[A'(u, \zeta)]^2}{A(u, \zeta)} \right] \frac{d}{d\zeta} \langle h^2 \rangle_\zeta \quad (A19)$$

$$\frac{\partial B}{\partial \zeta} = \frac{1}{2} \left[B''(u, \zeta) - \frac{A'(u, \zeta) B'(u, \zeta)}{A(u, \zeta)} \right] \frac{d}{d\zeta} \langle h^2 \rangle_\zeta \quad (A20)$$

where A and B are now scalar fields. Substituting (A14) in (A19) gives to second order in $\langle h^2 \rangle_\zeta$

$$a_1 + 2a_2 \langle h^2 \rangle_\zeta = -\frac{3}{2} + \frac{1}{2} \langle h^2 \rangle_\zeta (a_1'' - 6u^{-1} a_1' + 9a_1 u^{-2})$$

or

$$a_1 = -\frac{3}{2}u$$

$$a_2 = \frac{1}{4} (a_1'' - 6u^{-1} a_1' + 9a_1 u^{-2}) = -\frac{9}{8} u^{-1}$$

Thus, to second order

$$A = u^3 - \frac{3}{2} u \langle h^2 \rangle_\zeta - \frac{9}{8} u^{-1} \langle h^2 \rangle_\zeta^2$$

$$= u^3 \left(1 - \frac{3}{2} \frac{\langle h^2 \rangle_\zeta}{u^2} - \frac{9}{8} \frac{\langle h^2 \rangle_\zeta^2}{u^4} \right)$$

In a similar way one obtain to second order

$$B = u \left(1 - \frac{3}{2} \frac{\langle h^2 \rangle_\zeta}{u^2} - \frac{21}{8} \frac{\langle h^2 \rangle_\zeta^2}{u^4} \right)$$

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