

## JULICH The role of the anion exchange membrane RNTHAACHEN thickness for CO<sub>2</sub> electroreduction in direct formic acid electrolysis



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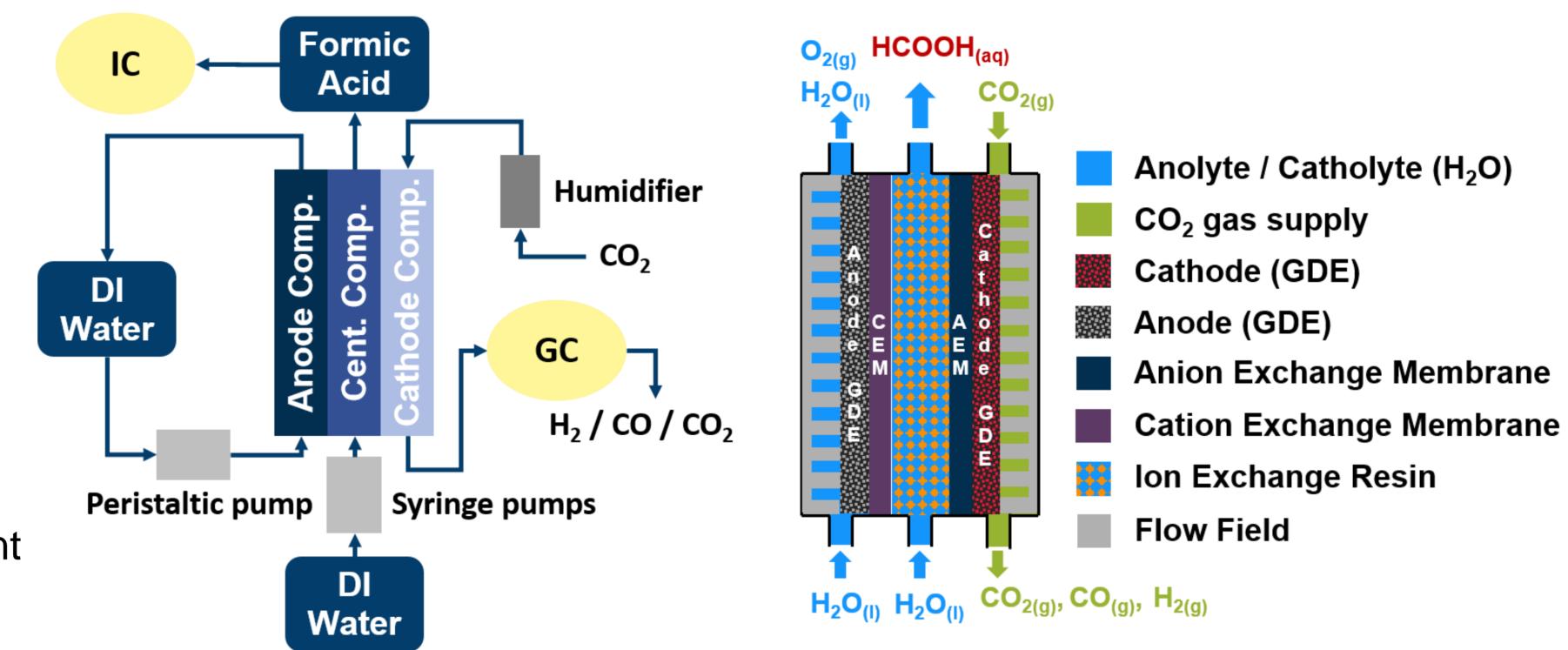
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### Introduction

The implementation of a closed carbon cycle by 'Power-to-X' (P2X) technologies is of great interest aiming at a CO<sub>2</sub> neutral economy. Especially formic acid is a relevant product of P2X processes, since it can be produced selectively and efficiently using earth-abundant catalysts. This study focuses on the investigation of a three-compartment flow cell, which allows to produce formic acid, instead of formate. Here, the electrolyzer performance using PiperION membranes of various thicknesses ranging from 13 – 80 µm is evaluated. [1 - 2]

## Experimental Setup

- Experimental Parameters:
- Active electrode area: 5 cm<sup>2</sup>
- Flow rate center compart.: 0.1 mL min<sup>-1</sup>
- $CO_2$  supply: 60 mL min<sup>-1</sup> ( $\lambda = 8.0$ )
- Flow rate anolyte: 3.0 mL min<sup>-1</sup>
- AEM: PiperION (A13, A22R, A35, A80)
- CEM: Nafion 324
- GDEs: Custom-made GDEs
- The ion exchange resin in the center compartment allows for a direct production of formic acid



## GDE Preparation

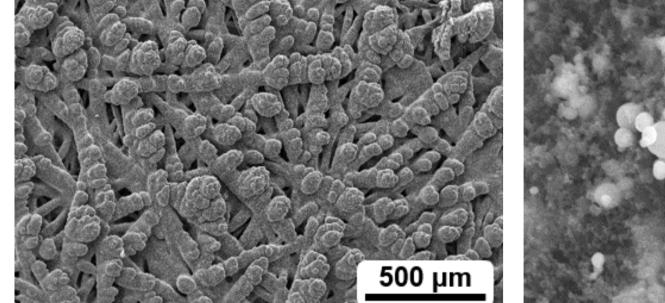
# Ink preparation Spray-coating

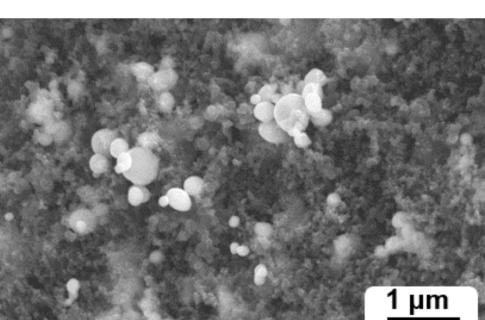
Catalyst: Bi<sub>2</sub>O<sub>3</sub> Binder: PiperION

Additive: Carbon powder Ultrasonication Dispersion medium: Ethanol

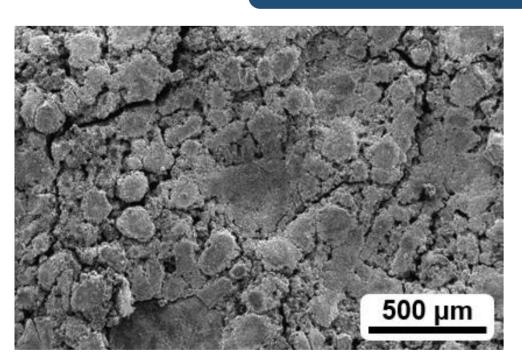
> **Substrate:** TP120 (30%) Catalyst loading: 4 mg cm<sup>-2</sup>

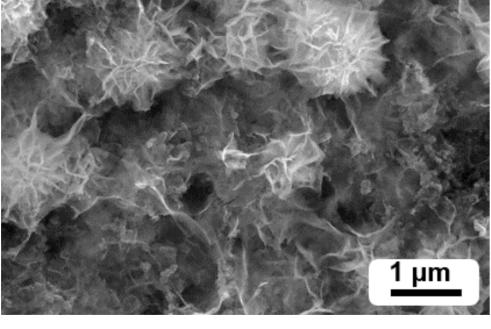
### GDE as prepared



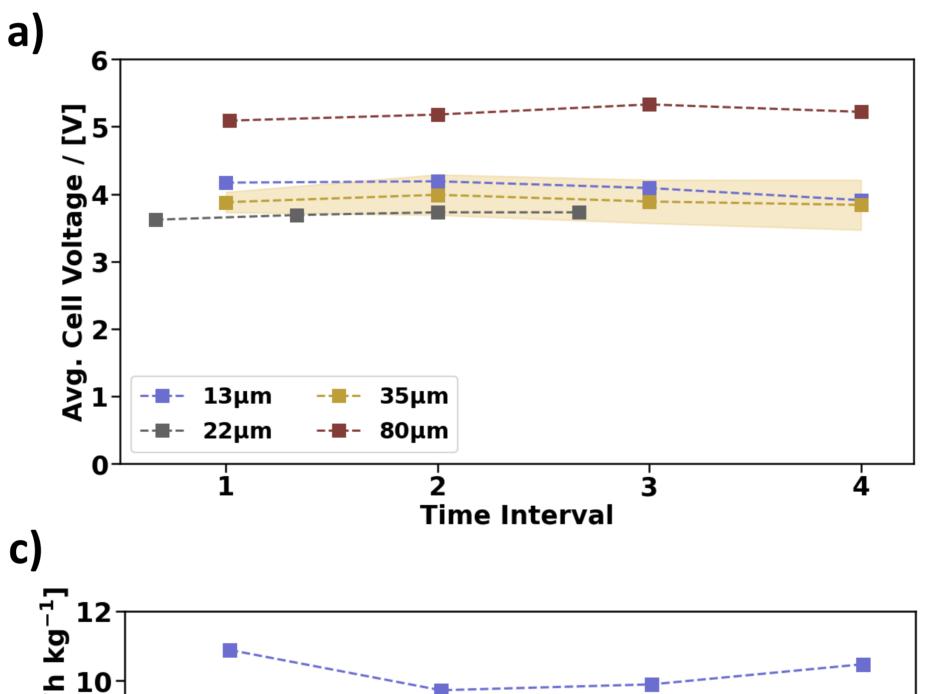


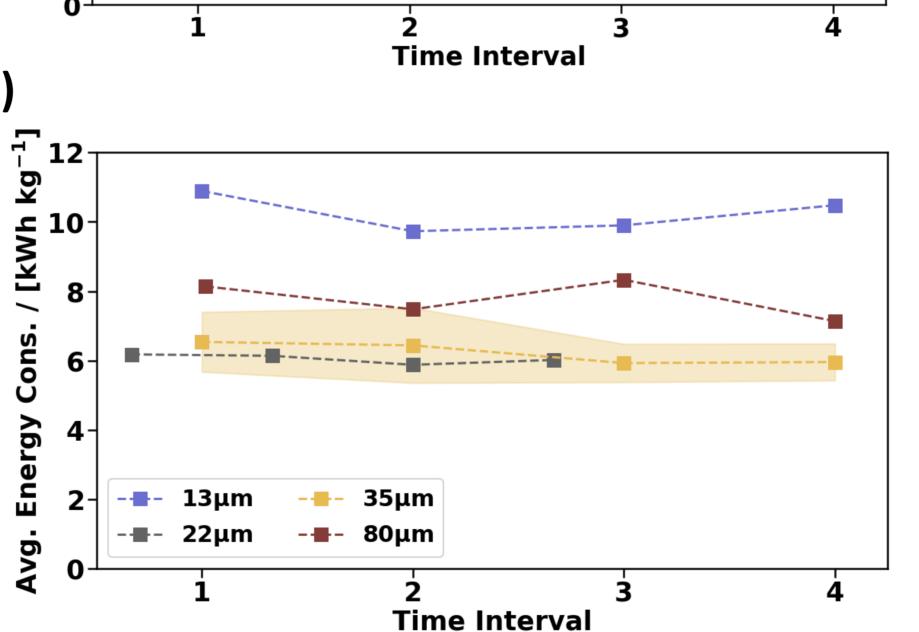
#### GDE after electrolysis

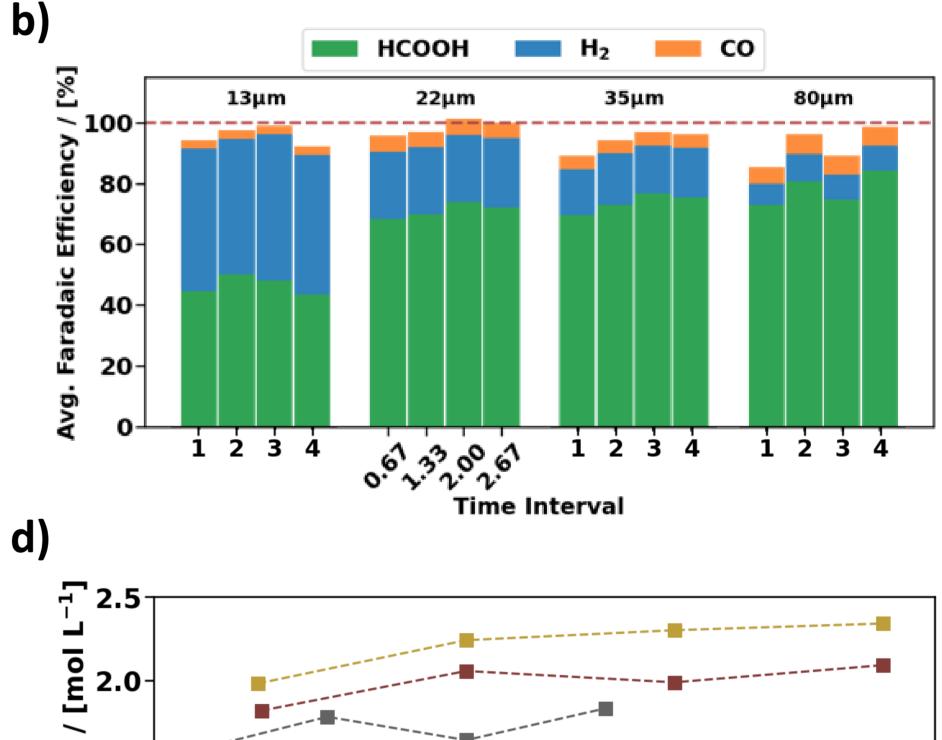


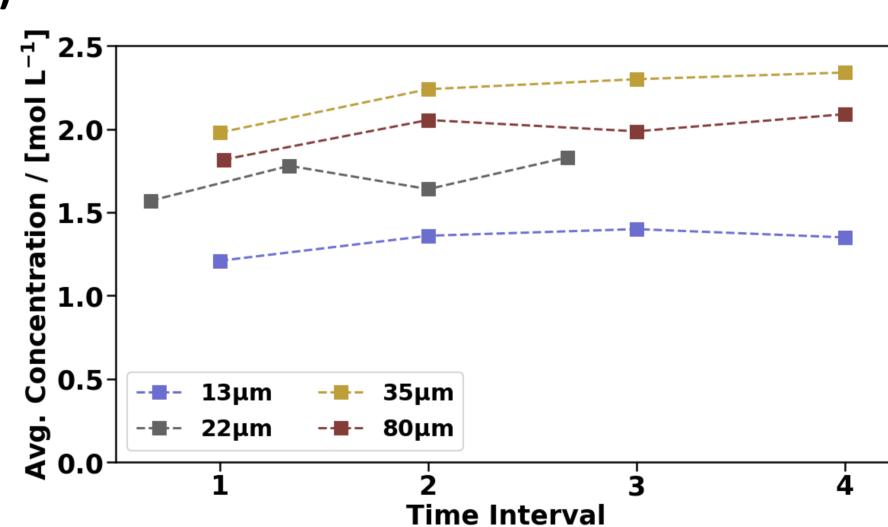


### Results









Electrolyzer performance for CO<sub>2</sub> electroreduction to formic acid depending on the AEM thickness during up to 4 hours of continuous testing at 200 mA cm<sup>-2</sup>. a) Average cell voltage, b) average faradaic efficiency of formic acid, H<sub>2</sub> and CO, c) average energy consumption and d) average concentration of resulting formic acid.

### Conclusion

The performance of a three-compartment flow cell for direct formic acid production by CO<sub>2</sub> electroreduction using 13 µm, 22 µm, 35 µm and 80 µm thick PiperION anion exchange membranes was investigated for up to 4 hours. Within this study, the best results in terms of electrolysis performance were obtained for PiperION (35 µm), which allowed up to 76%, about 6.0 kWh kg<sup>-1</sup> and 2.3 mol L<sup>-1</sup>, respectively. Similar values, except for a lower formic acid concentration, were obtained for PiperION (22 µm). In contrast, PiperION (80 µm) lead to high cell voltages above 5 V and PiperION (13 µm) showed very low faradaic efficiencies for formic acid with around 45%. Thus, there is no linear correlation between membrane thickness and cell performance. This suggests a superimposition of various effects.





**Acknowledgment:** The authors kindly acknowledge funding by the Federal Ministry of Education and Research (BMBF).

Project: iNEW2.0 'Inkubator Nachhaltige Elektrochemie' Funding code: 03SF0627A

[1] H. Yang et al., J. CO2 Util., vol. 20, 208–217, 2017. [2] J. M. Spurgeon et al., Energy Environ. Sci., vol. 11, 1536–1551, 2018.