

# The effect of shear-induced migration on crossflow filtration of colloids

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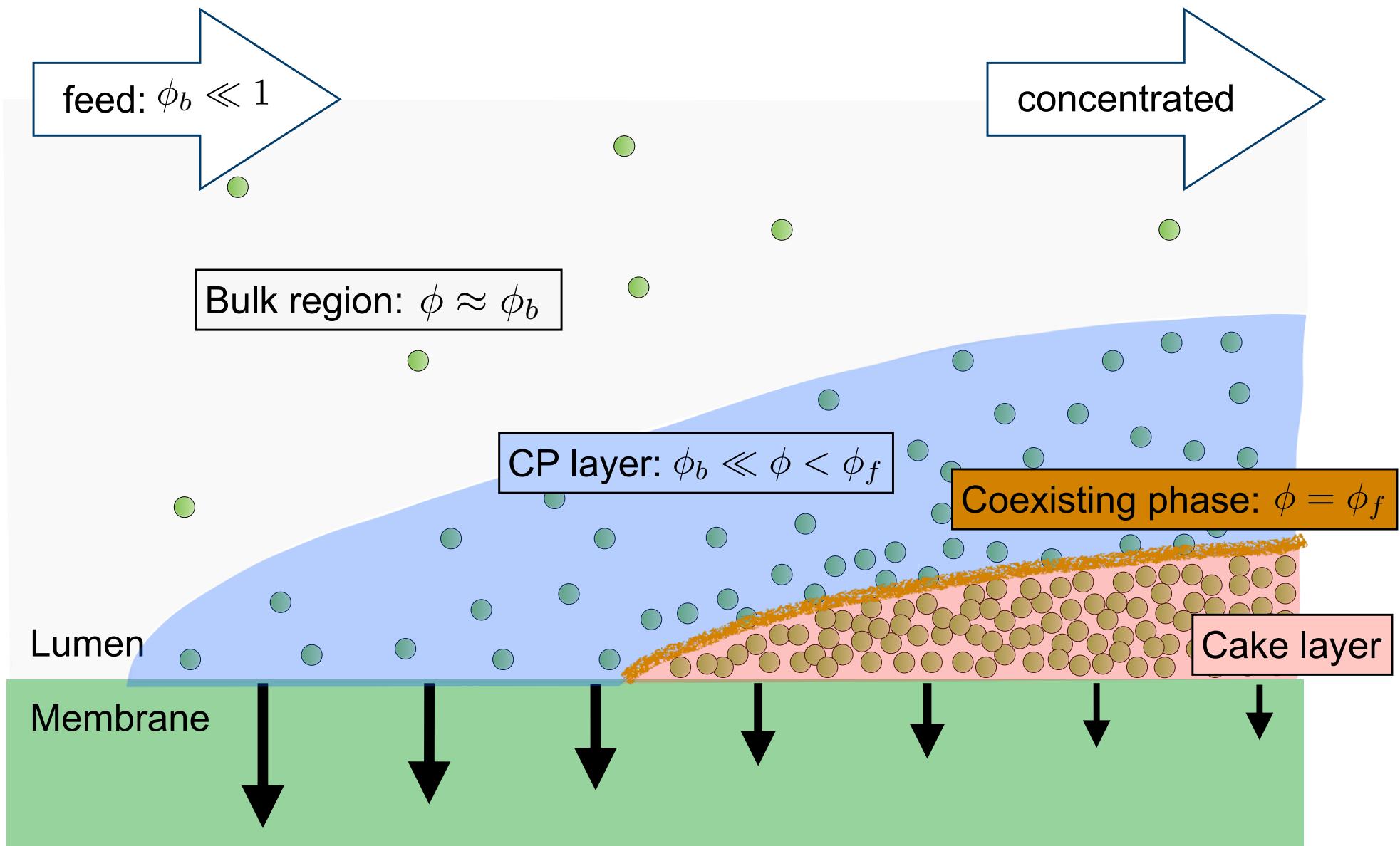
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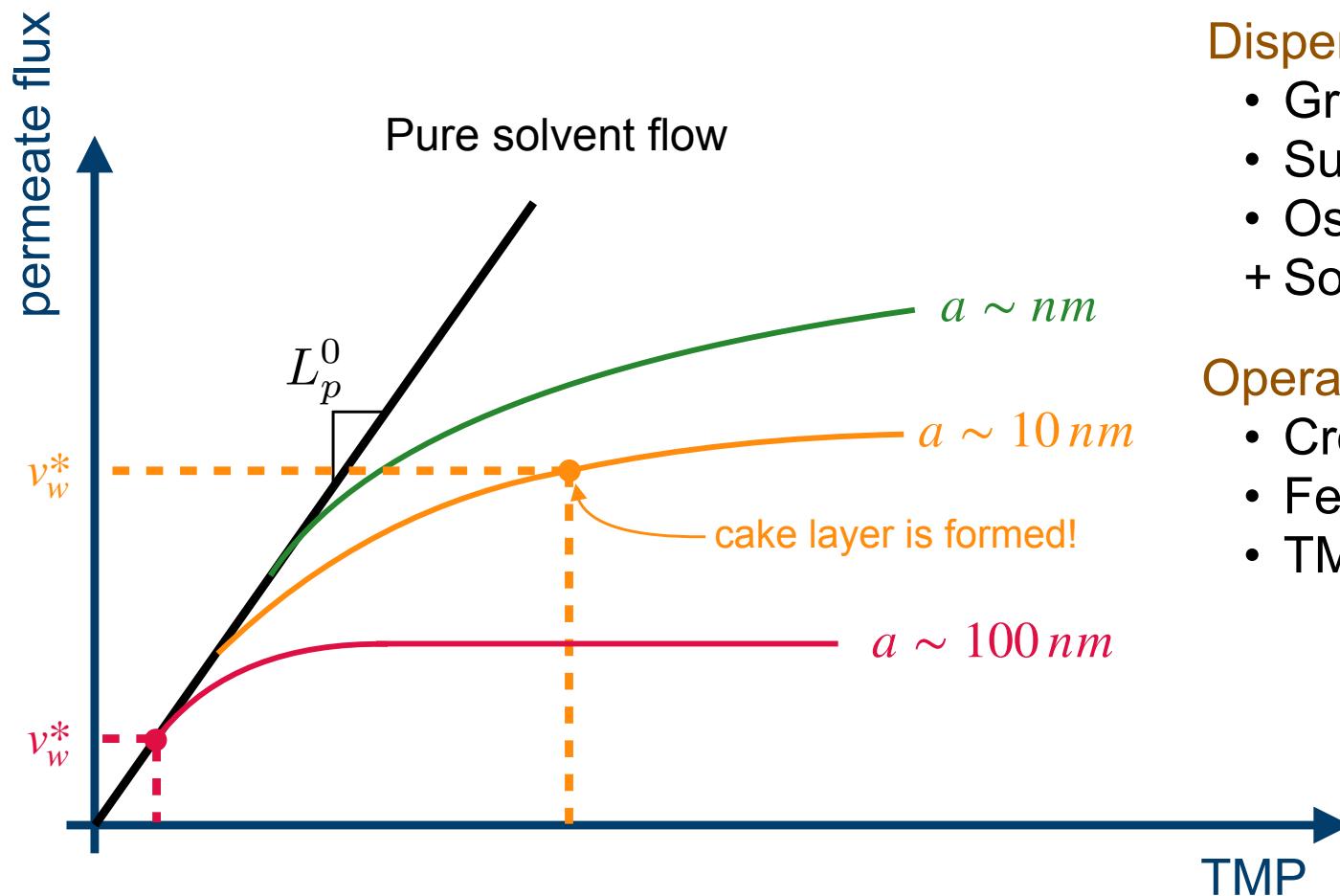
## References:

1. Park and Nägele, *JCP*, 2020
2. Park and Nägele, *Membranes*, 2021
3. Park, Dhont, and Nägele (manuscript in preparation)

# Crossflow filtration



# Conditions for cake layer formation



**Membrane properties:**

- Hydraulic permeability
- Membrane dimensions

**Dispersion properties:**

- Gradient diffusion coefficient
- Suspension viscosity
- Osmotic pressure
- + Solidification (cake layer)

**Operating conditions:**

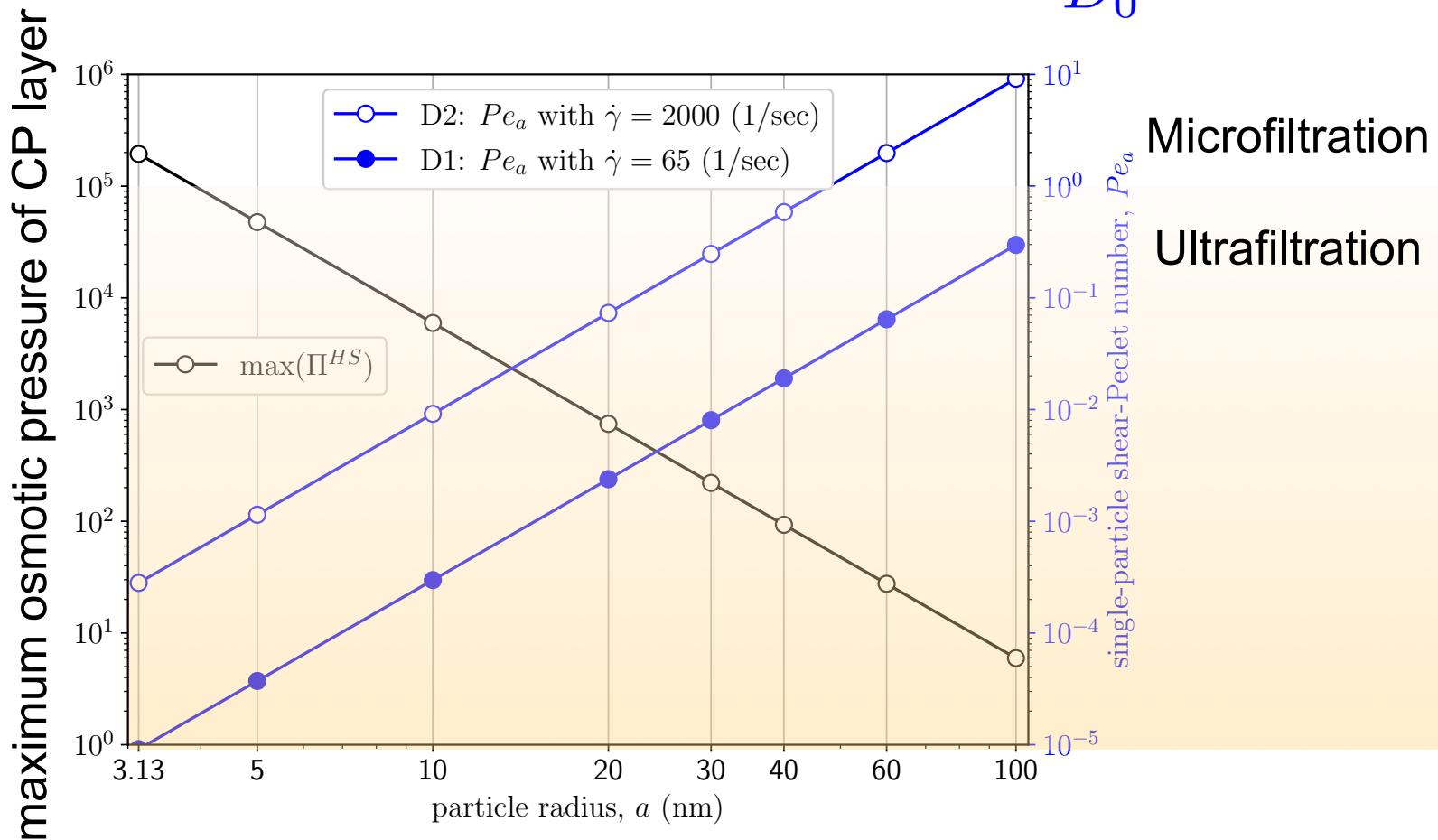
- Crossflow velocity
- Feed concentration
- TMP

# Effect of particle size

## Ultrafiltration and microfiltration

$$\Pi(\phi_f; a) = \frac{k_B T}{(4/3)\pi a^3} \phi_f Z(\phi_f) \propto \frac{1}{a^3}$$

$$Pe_a = \frac{\dot{\gamma} a^2}{D_0} \propto a^3$$



# mBLA method

Park and Nägele, *JCP*, 2020  
 Park and Nägele, *Membranes*, 2021

## CF model

Advection-diffusion equation ( $\phi$ )

Effective Stokes equation ( $\mathbf{V}, P$ )

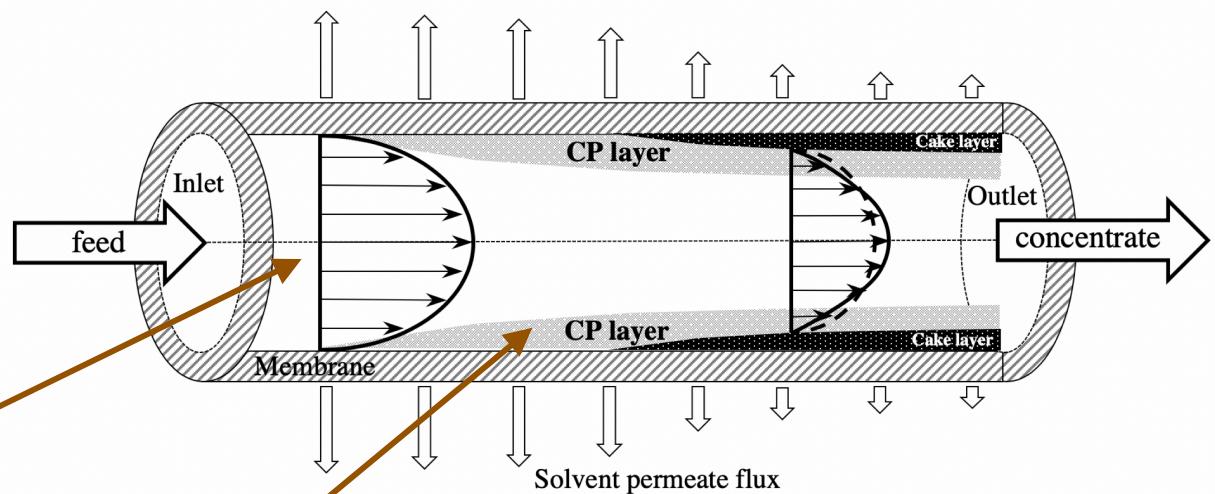
Darcy-Starling equation ( $v_w$ )

## Bulk (outer) solution

- $\phi^{out}(y, z) \approx \phi_b$  (about  $10^{-3} \sim 10^{-4}$  in this study)
- Similar to pure solvent flow profile (except  $v_w$ )

## Boundary layer (inner) solution

- Wall concentration  $\phi_w$  can be up to  $\phi_f \approx 0.494$ .
- Strong influence of  $(\phi, \dot{\gamma})$  on dispersion properties



$$k^2 = 16 \left( \frac{L}{R} \right)^2 \frac{\eta_s L_P^0}{R}$$

$$Pe_R = \frac{v_w R}{D_0} \gg 1$$

+ Global particle flux conservation law  $\Rightarrow \phi_w(z)$  and  $L_p(z)$

Note: mBLA method provides

- semi-analytic expression for  $(\mathbf{V}, P, \phi)$  inside lumen
- In good agreement with FEM result (and fast!)

# Simplified relation: flux and concentration

**without non-linear axial variation of flow profile, osmotic pressure, and cake at outlet**

$$k^2 \ll 1$$

$$\Pi/\text{TMP} \approx 0$$

$$\phi_w(z = L) = \phi_f$$

$$\text{Eq. } (*) \dots \quad \frac{Pe_R^*}{\Psi^{1/3}(Pe_R^*)} \approx \left[ 2 Pe_L \frac{\phi_f}{\phi_b} \right]^{1/3}$$

$$Pe_R^* = \frac{R^2/D_0}{R/v_w^*}$$

$$Pe_L = \frac{R^2/D_0}{L/u^0}$$

## Effect of different dispersion properties:

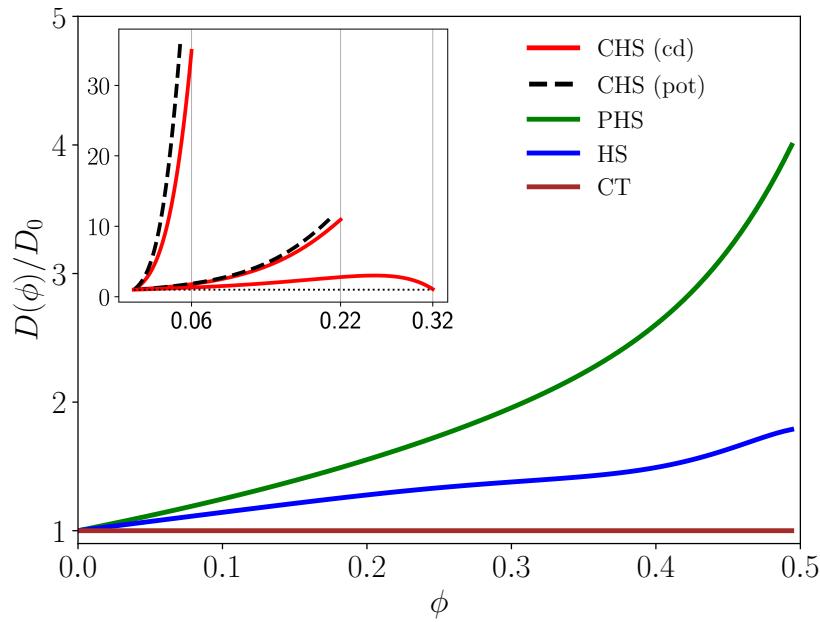
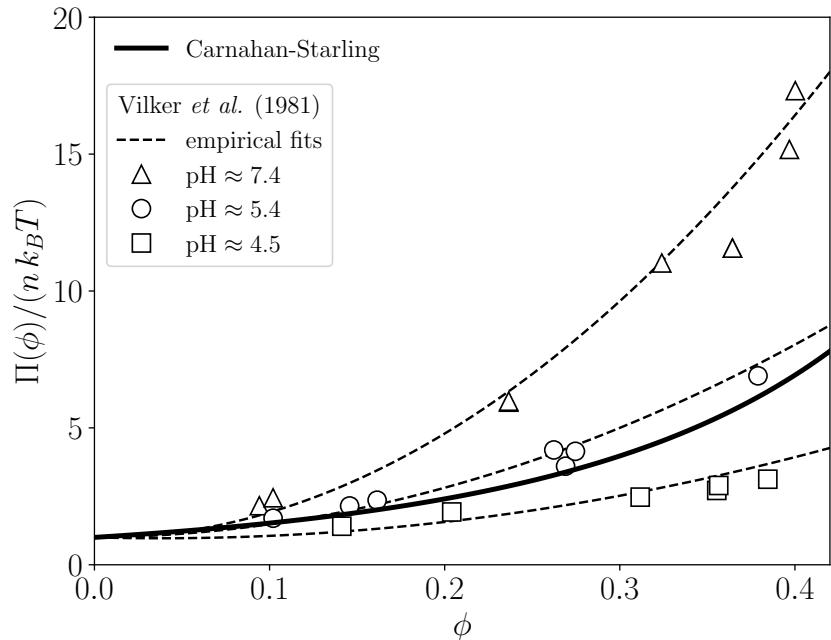
$$\Psi(Pe_R^*) \approx \frac{(Pe_R^*)^2}{2} \int_0^1 d\tilde{y} (1 - \tilde{y})(2 - \tilde{y}) \left( \frac{1}{\eta^*} \int_0^{\tilde{y}} \frac{\eta_s}{\eta(\phi)} d\tilde{y}' \right) \exp \left( -Pe_R^* \int_0^{\tilde{y}} \frac{D_0}{D(\phi)} d\tilde{y}' \right)$$


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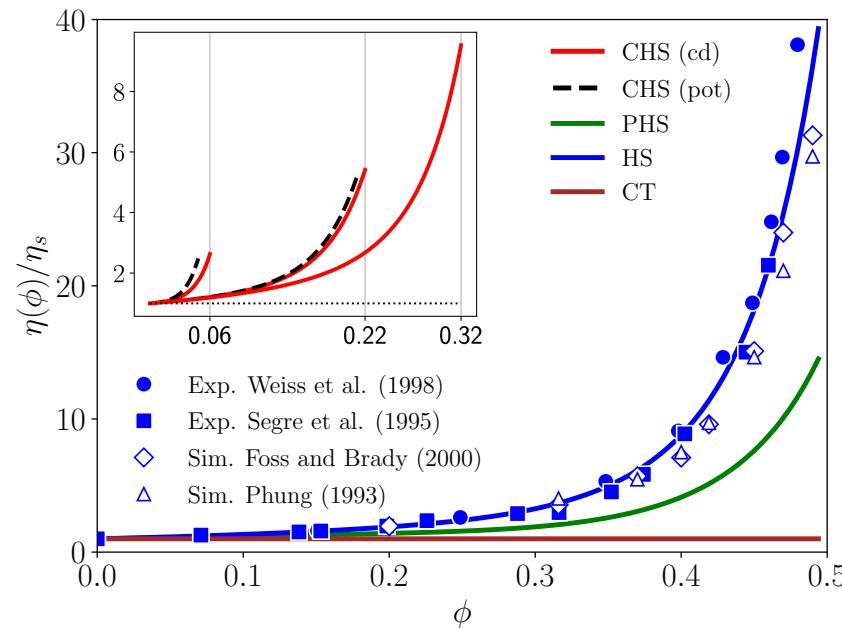
viscosity effect  
(from axial velocity)
diffusivity effect  
(from concentration)

- For constant transport properties (CT):  $\Psi^{CT}(Pe_R^*) \approx 1$
- Similar to standard earlier description of CT (film theory + mass transfer coefficient)

# Equilibrium dispersion properties

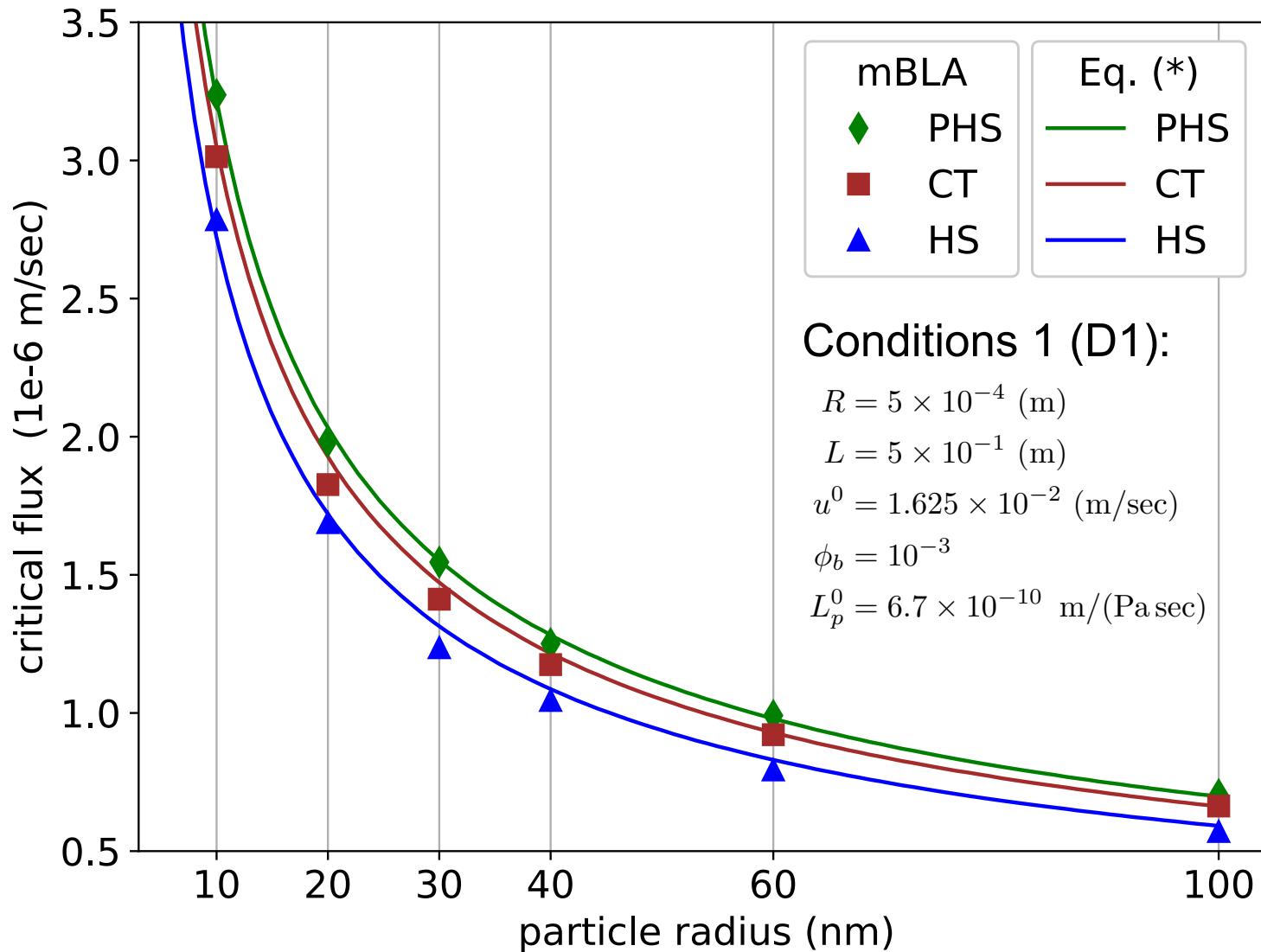


We stay focused on the neutral dispersions:  
 HS = hard spheres  
 PHS = solvent-permeable hard spheres  
 CT = constant transport properties



# Critical flux vs. particle size

PHS/CT/HS under conditions 1 (D1)



# Shear-induced diffusivity ( $Pe_a \lesssim 10$ )

- At equilibrium freezing concentration:  $\phi_f = \phi_f^{eq}$
- No osmotic pressure contribution:  
 $40 \text{ nm} \leq a \leq 200 \text{ nm}$   $\frac{\Pi(\phi_f, Pe_a)}{\text{TMP}} \approx 0$
- Without shear-thinning effect:  $\eta = \eta^{KD}(\phi)$
- Equilibrium sedimentation coefficient:  $K_{sed} = K_{sed}^{eq}(\phi)$
- Shear-curvature effect is negligible:  

$$-j_y^{diff} = D_{yy}(\phi, \dot{\gamma}) \frac{\partial \phi}{\partial y} + \xi(\phi, \dot{\gamma}) \cancel{\frac{\partial \dot{\gamma}}{\partial y}}$$
- yy-component collective diffusion tensor:

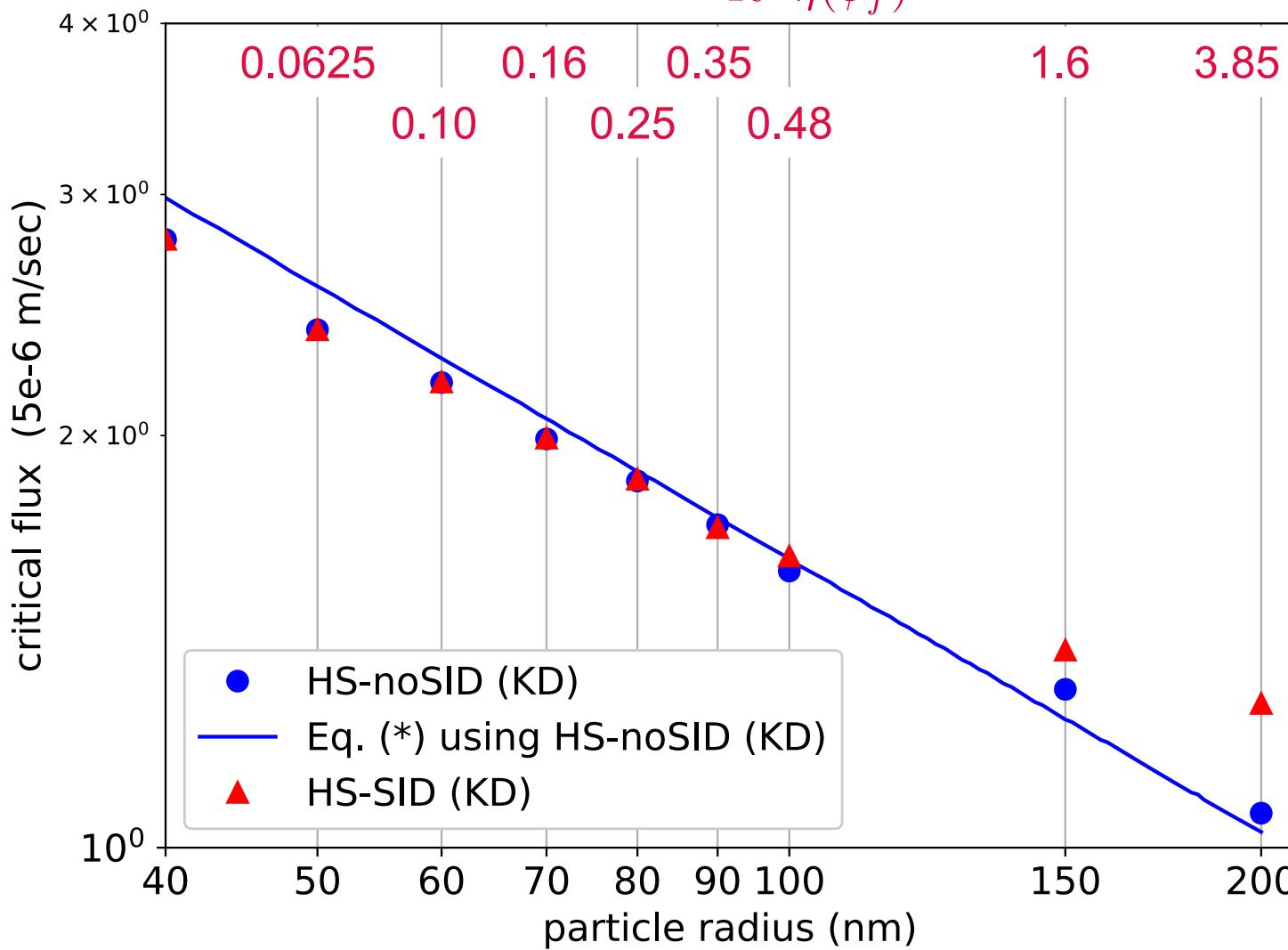
$$D_{yy}(\phi, Pe_a) = D_0 K_{sed}^{eq}(\phi) \left[ 1 + 4 \frac{\partial}{\partial \phi} (\phi^2 g_{iso}^c(\phi, Pe_a)) \right]$$

Jin ... Dhont, *JCP* (2014)

# Effect of shear-induced diffusivity

HS in equilibrium, HS with SID

$$Pe_a(y = 0, z = L) \approx \frac{2u^0}{R} \frac{1}{\eta(\phi_f)}$$



Condition 2 (D2):

$$R = 1 \times 10^{-4} \text{ (m)}$$

$$L = 5 \times 10^{-2} \text{ (m)}$$

$$u^0 = 0.1 \text{ (m/sec)}$$

$$\phi_b = 10^{-4}$$

# Concluding remarks

- Concentration-polarization and cake layers are important filtration subjects
- Predicting the critical flux is a long-standing key problem not fully solved to date
- mBLA method provides accurate semi-analytic flow and concentration profiles
- Simplified critical flux result prediction in Eq. (\*) is accurate and related the new mBLA method to earlier less accurate methods
- Explore effect of shear-induced diffusivity on the critical flux
  - Work in progress: Shear-thinning and osmotic pressure effects

## References:

1. Park and Nägele, *JCP*, 2020
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# Thank you

Jan Dhont

Gerhard Nägele

I am here



Institute of Biological Information Processing (IBI-4), Forschungszentrum Jülich

SFB985: Functional microgel and microgel system



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